Physics II   2011

Ch 16   Temperature & Heat

Temperature: a <u>macroscopic</u> quantity or property (we can sense and measure) that is a consequence of <u>microscopic</u> behavior of matter. (energy)

↳ **Units:**

°F
(degree Fahrenheit)

(Body temp. ~100 °F)
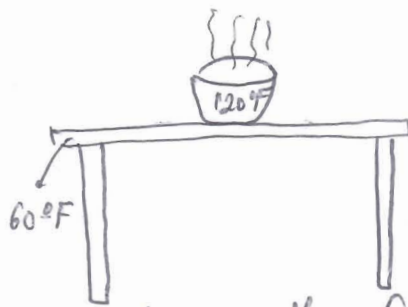
°K
(degree Kelvin)

↓

Absolute zero temp. is 0 °K

°C
(degree Celsius)

H_2O { Freezing : 0 °C
{ Boiling : 100 °C
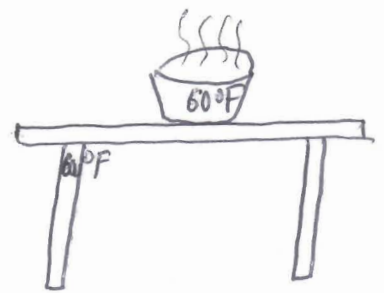↳ Normal conditions

$$T_F = \frac{9}{5} T_C + 32$$

$$T_C = \frac{5}{9}(T_F - 32)$$

$$T_C = T_K - 273.16°$$

Triple point of water
(3 phases coexist @ this temperature)

Hot bowl of soup
120 °F

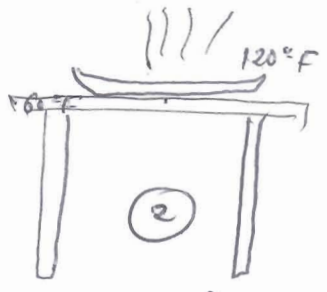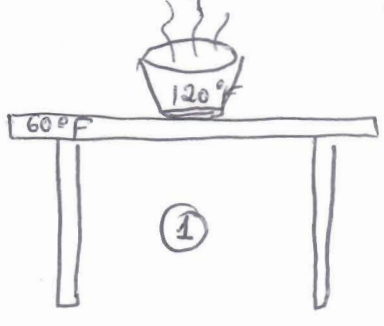Now it is in <u>thermal contact</u> with the table :
they can exchange heat

After 8 hours :
Temperature has changed, they have arrived at a thermodynamic equilibrium (T.D. equilibrium) :
1) $T_{final} = 60°F$ (since table is in thermal contact with the room)
2) By <u>exchanging heat</u>

<u>Heat exchange or transfer rate</u> (heat transfer per unit time): H

H: how fast heat can be transferred b/w two objects; let's describe
this quantitatively using our intuition:

① (bowl of soup at 120° on a table at 60°F)

② (wider plate at 120°F on table at 60°F)

$$H = -k \frac{A}{\Delta x} \Delta T$$

Thermal constant of material
heat needs to travel
through (hot matter)

→ Larger surface
area (in thermal
contact) → faster
heat transfer

→ Also: faster heat
transfer if plate
or/and table were metal: → (free electrons → energy carriers)
thermal constant k   (Temperature is a consequence
of microscopic properties)
of matter

③ (thicker table, Δx)

(bowl at 120° on table over ice at 60°)

larger thickness Δx
↓
Slower heat transfer
rate!

larger (ΔT)
(b/w soup & table)
→ faster heat transfer

<u>Thermal constant k:</u>

Glass windows :   k

Single pane   Double pane

hotter | colder
(outside)

(single pane) ↓
halves H

Glass | Glass
↓
air
↓
more than
halving H

→ But some gas is needed b/w layers
to hold against atmospheric pressure.

Microscopic connection:
→ Air is poorer heat conductor
b/c its lower density.

Units for H:

Quantity	Dimensions	S.I. unit
Length	L	meter (m)
Mass	M	kilogram (kg)
Temperature	T }	degree Kelvin (°K)
Time	T }	second (s)
Energy	$\dfrac{ML^2}{T^2}$	joule (J)

↳ Mechanical: kinetic, potential
Thermal or heat

Power	$\dfrac{ML^2}{T^3}$	$\dfrac{joule}{s}$ = Watt (W)

Dimension for H:

$$[H] = [k][A]\frac{[\Delta T]}{[\Delta x]}$$

$\downarrow \qquad\qquad \downarrow$

$\dfrac{J}{s} = W \qquad m^{\ell} \cdot \dfrac{°K}{m}$

$\longrightarrow$ Unit = $\begin{cases} \dfrac{W}{m \cdot °K} & (SI) \\[2mm] \dfrac{Btu \cdot \widehat{in}}{h \; ft^2 \; °F} & (British) \end{cases}$

k

→ inch

$\downarrow$
hour

$\mathcal{R}$-factor or another way of writing H: $\mathcal{R} = \dfrac{\Delta x}{k}$
(curly R)

$$\left[H = -\left(k\,\frac{A\,\Delta T}{\Delta x} \right) = -\frac{A\,\Delta T}{\mathcal{R}} \right]$$

→ Commonly used in insulator materials: (↑ $\mathcal{R}$ are more expensive and better insulator):

$\mathcal{R}-21$ means: $\mathcal{R} = 21 \dfrac{ft^2 \; °F}{\frac{Btu}{h}}$

Mechanisms of Heat Transfer:

← pan with water
stove top

Initially: turn on stove, stove top is heated, then heat gets transferred into water at bottom of pan: heat transfer by |conduction| (via free electrons in bottom of metal pan).
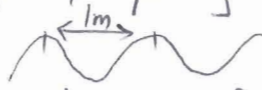
Water at bottom of pan gets heated, then water at top of pan gets heated: heat transfer by |convection| (in fluid: liquid or gas).

Air convection: { heaters: located low : hot air will rise & cold air will sink.
AC's: located high to allow the air convection.
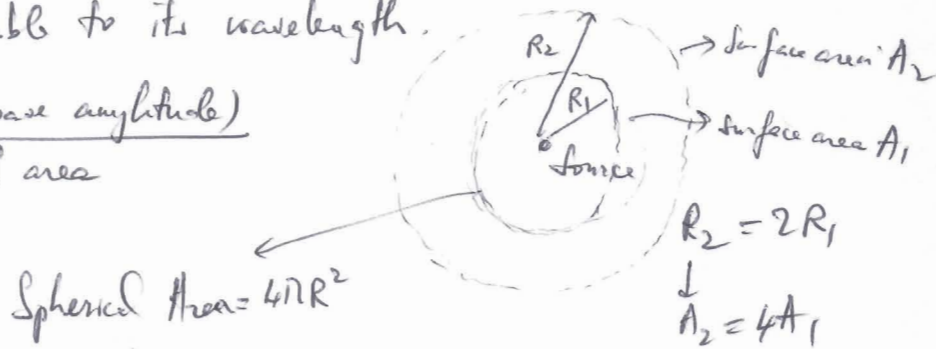so all parts of a room can be at a same temperature.

When placing your hand next to pan you feel the heat → by |radiation|
Does it require a medium with matter?

Sound waves need a medium: air

Radiation such as solar light requires no medium to propagate: EM (electromagnetic) waves (infrared, microwaves, lights, depending on their wavelengths)

Radiowaves: $\lambda \sim 1m$ Can't get a good signal sufficiently far from station: because of reflections & interferences with structures of sizes comparable to its wavelength.

Intensity = $\dfrac{\text{strength (wave amplitude)}}{\text{unit area}}$

Spherical Area = $4\pi R^2$

$R_2 = 2R_1$
$\downarrow$
$A_2 = 4A_1$

→ surface area A_2
→ surface area A_1

→ intensity goes down 4 fold as the radius is doubled
→ from spherical geometry (not wave reflections or interferences)
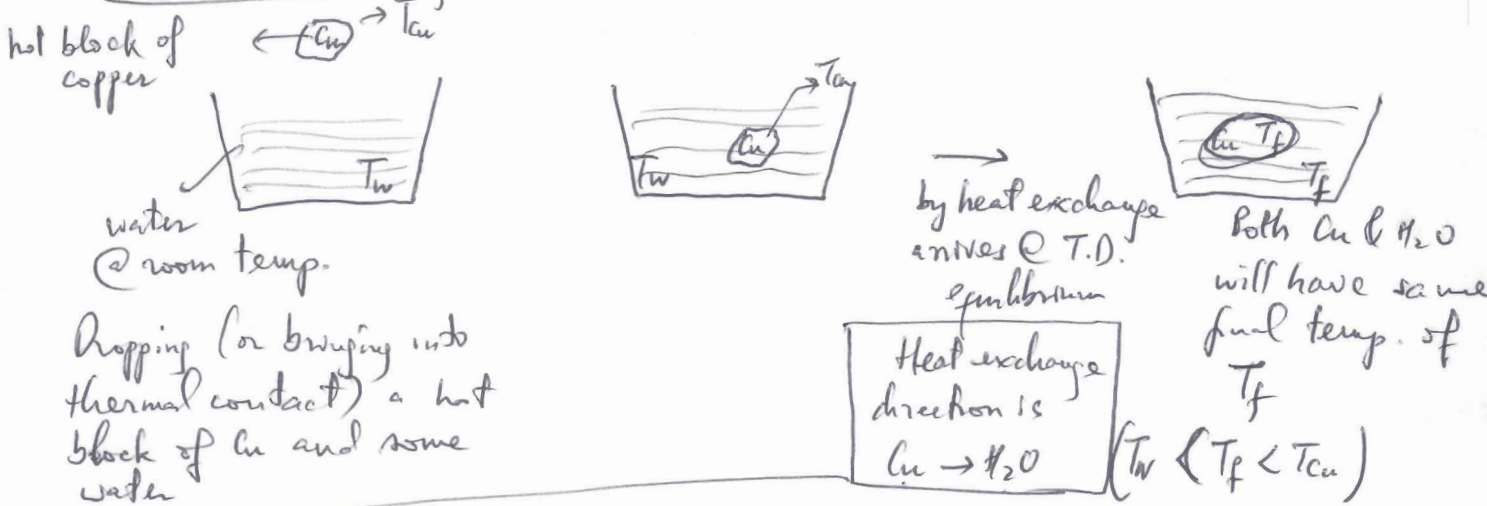
<u>Convection</u>: in fluids there was a phenomenon we can take advantage for transportation. in air and in water (hot air balloons and ships:) bouyancy (lower density stays above higher density)

<u>Radiation</u>: Stefan - Boltzman law: heat loss rate by radiation of an object of area A & temperature T

$$\underset{\downarrow}{P} = \underset{\downarrow}{e} \quad \sigma \quad A\;\boxed{T^4}$$

energy loss per unit time or power

emissivity coefficient

'sigma' or Stefan-Boltzman constant $5.67 \times 10^{-8} \dfrac{W}{m^2\,{}^\circ K}$

Heat Balance Equations:

hot block of copper

$\leftarrow \boxed{Cu} \rightarrow T_{cu}$

water @ room temp.

T_w

Dropping (or bringing into thermal contact) a hot block of Cu and some water

$\rightarrow T_{cu}$

Cu

T_w

by heat exchange arrives @ T.D. equilibrium

Heat exchange direction is

$Cu \rightarrow H_2O$

$Cu\;T_f$

T_f

Both Cu & H_2O will have same final temp. of T_f

$(T_w < T_f < T_{cu})$

$$\underset{\substack{\text{Heat loss}\\\text{by Cu}\\\text{negative}}}{\underline{\Delta Q_{cu}}} + \underset{\substack{\text{Heat gain}\\\text{by } H_2O\\\text{positive}}}{\underline{\Delta Q_w}} = 0$$

(Assuming system water & Cu is isolated)

(Heat left Cu went into H_2O)

$$m_{cu}\,\underset{\substack{\text{specific heat}\\\text{of Copper}}}{C_{cu}} (T_f - T_{cu}) + m_w\, C_w (T_f - T_w) = 0$$

specific heat : capacity to absorb heat per unit mass : specific to the material.

$C_w = 4184 \dfrac{J}{kg\,{}^\circ K}$

$C_{cu} - 386 \dfrac{J}{kg\cdot}$

ch 17 Thermal Behavior of Matter

	Density	State
Matter can exist in 3 states {	low	Gas : almost free molecules (not interacting)
	Medium	liquid: some interaction b/w molecules
	High	Solid : molecule / atoms are not free move.

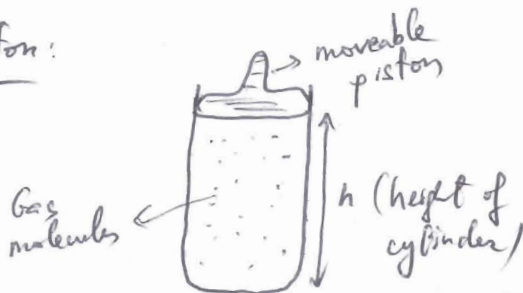Microscopic properties will influence / determine macroscopic thermal behavior.

Thermal Behavior of Gases :
- Ideal gases → molecules are completely free!
- Real gases → some interaction b/w molecule

Ideal Gases
{ Microscopic : N molecules or particles

Macroscopic behavior { T (Temp, °K)
P (Pressure, Pa)
V (Volume, m³) }

Piston :

→ moveable piston

Gas molecules

h (height of cylinder)
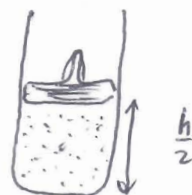
state ① T, P, V N

Assume { a) No gas leaking

b) Compression is done VERY slowly.
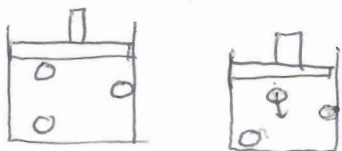So little energy is transferred to molecules which is dissipated out
↳ isothermal process

State ② : $T, 2P, \frac{V}{2}$ N

$\frac{h}{2}$

→ Observations { $P \cdot V$ is the same in ① & ②
$N \cdot T$ is also the same in ① & ② }

$PV = \textcircled{k} NT$
$k = $ Boltzman constant $= 1.38 \times 10^{-23} \frac{J}{°K}$

If we go slow enough we may hit any molecule → no additional KE for molecule. Although they will hit each other more frequently due to reduced volume they didn't receive any extra KE. (or may have enough time to transfer it back to the container)

Avogadro number: $N_A = 6.022 \times 10^{23}$

$N = n \cdot N_A$: $n =$ number of moles

Ideal gas equation

$$P \cdot V = K N T = k n N_A T = n \, k N_A \, T = n R T$$

$$\boxed{R = 8.314 \, \frac{J}{^\circ K \, mol}}$$

$$\boxed{P \cdot V = n R T}$$ (Ideal gases where there is no interaction b/w molecules)

Real gases: With some interaction b/w molecules:

$$\left(P + \frac{n^2 a}{V^2} \right) (V - nb) = n R T$$

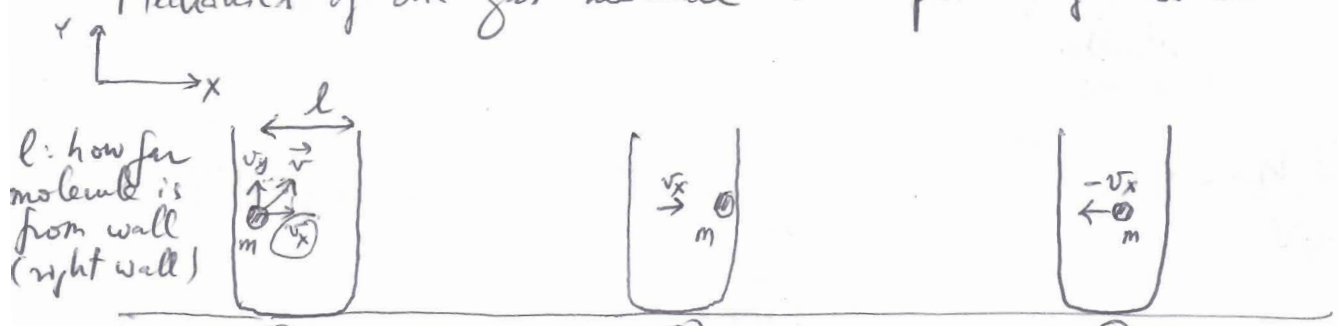a, b are given constants, depending on the strength of interactions b/w molecules.

A closer look at   microscopic behavior & macroscopic properties.

↳ quantitative

Transfer of momentum
b/w gas molecule &
container

Temperature, Pressure

Mechanics of one gas molecule :   a particle of mass m

$y \uparrow$
$\llcorner \rightarrow x$

l: how far
molecule is
from wall
(right wall)

①   ②   ③

- Molecule travels in
  some direction inside
  a container.
- In term of momentum transfer
  to container → look at v_x!
  Molecule moving toward right
  wall @ v_x

- Hits right wall
- Elastic collision ⟶

↳ - Rebounds with
    same speed in opposite
    direction

$\boxed{\text{System}}$ =   gas molecule + container

Net external force on system :   in x-direction : $F_{net,x} = 0$
(mg is along y-direction)

2nd Newton's ⟶ ''
       law $\dfrac{dp_x}{dt} = 0$

→ $\boxed{\begin{array}{c} P_x \text{ of system is} \\ \text{conserved} \end{array}}$

Before collision
     ①

After Collision
     ③

$$m v_x + \underbrace{M \cdot 0}_{0} = -m v_x + \boxed{\underbrace{M v_{x_{f,c}}}_{\underset{\textstyle \overset{||}{②m v_x}}{}}}$$

After the elastic collision the molecule has transferred $2 m v_x$
of momentum to the container :

Pressure: $P_i = \dfrac{F_i}{A} = \dfrac{\frac{\Delta p_i}{\Delta t}}{A} = \dfrac{\frac{2m\,v_x}{\frac{2\ell}{v_x}}}{A} = \dfrac{m\,v_x^2}{\boxed{A \cdot \ell}} = \dfrac{m\,v_x^2}{\text{Vol.}}$

by one molecule
↳ force applied
per unit area

Volume

Pressure due to N molecules $\quad P = \displaystyle\sum_{i=1}^{N} P_i = \dfrac{m}{\text{vol}} \sum_{i=1}^{N} v_{x_i}^2$

↓
all molecules
have the same
mass

Total pressure $\quad P = \dfrac{mN}{\text{vol}} \dfrac{\displaystyle\sum_{j=1}^{N} v_{x_j}^2}{N} \qquad\qquad \rightarrow P = \dfrac{mN \,\overline{v_x^2}}{V_{\leftarrow \text{vol.}}}$

$\underbrace{\qquad\qquad}_{\text{average of } v_x^2 \,=\, \overline{v_x^2}}$

$\rightarrow \boxed{P.V = mN \,\overline{v_x^2} = mN \dfrac{\overline{v^2}}{3}}$ (2) This came from $\boxed{\begin{array}{l} F = \dfrac{\Delta p}{\Delta t} \ 2^{nd}\text{Newton} \\ \text{Transfer of moment.}\end{array}}$

In general v_x is one othe three
components of the velocity $\vec{v}$ $\Big\} \rightarrow \boxed{\overline{v_x^2} = \dfrac{1}{3}\,\overline{v^2}}$
of magnitude v $\qquad\qquad\qquad$ Mathematically

Compare this with ideal gas equation: $\boxed{PV = kNT}$ (1)

$\rightarrow$ RHS's are equal! $\qquad kNT = mN\dfrac{\overline{v^2}}{3}$

$\qquad\qquad\qquad\qquad 3kT = m\,\overline{v^2}$

$\qquad\qquad\qquad \dfrac{3}{2}kT = \dfrac{1}{2}m\,\overline{v^2}$

$\boxed{\begin{array}{c} \downarrow \\ \text{Gas} \\ \text{Temperature} \\ \downarrow \\ \text{Macroscopic} \end{array}} \boxed{\begin{array}{c} \text{Average KE per} \\ \text{gas molecule} \\ \downarrow \\ \text{Microscopic} \end{array}}$

$\boxed{\begin{array}{l} \text{The microscopic average KE per molecule} \\ \text{determines the macroscopic temperature} \\ \text{of the gas} \end{array}}$
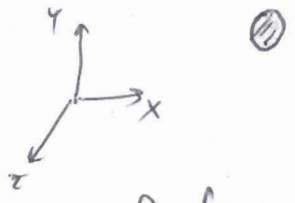
Dimensions & Degrees of Freedom (d.o.f)

3D: $\longrightarrow$ $\frac{3}{2}kT = \frac{1}{2}m\overline{v^2}$ $\begin{cases}$ Average KE per molecule in 3D is $\frac{3}{2}kT$ $\end{cases}$
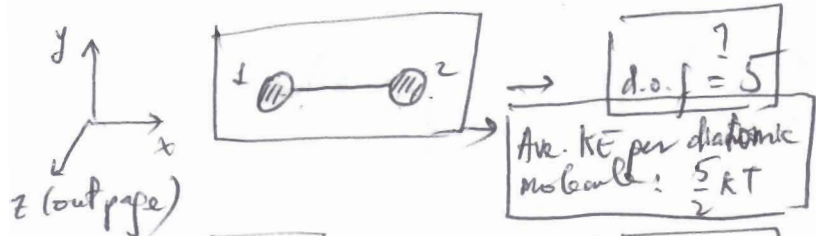
What is the average KE per molecule in **1D** in term of the gas temperature? $\frac{1}{2}kT \rightarrow$ | Average KE per molecule per dimension or d.o.f is $\frac{1}{2}kT$ |

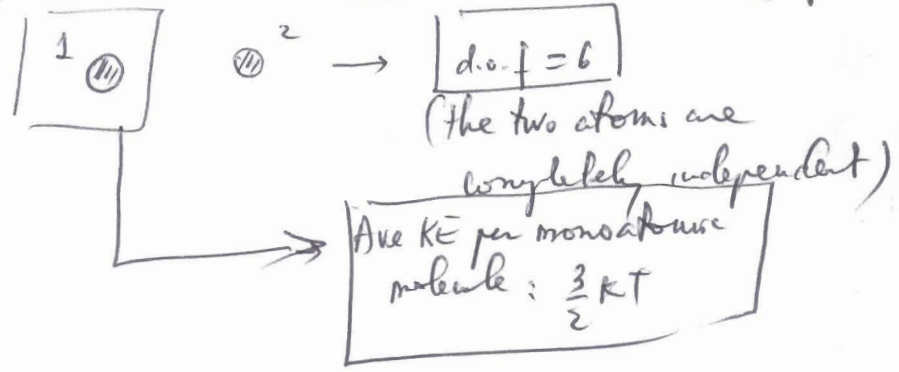What is the average KE per molecule in 2D? kT

Single molecules: or <u>monoatomic</u> molecules: $\rightarrow$ d.o.f = 3
one atom

Diatomic molecule (e.g. O_2) : two-atom molecule

$\rightarrow$ | d.o.f = 5 |

Ave. KE per diatomic molecule: $\frac{5}{2}kT$

$1 \rightarrow \begin{cases} x\text{-direction:} & \text{① moves right} \\ & \text{so will ②} \end{cases}$

$2 \rightarrow \begin{cases} y\text{-direction:} & \text{① moves up,} \\ & \text{② will not necessarily} \end{cases}$

$2 \rightarrow \begin{cases} z\text{-direction:} & \text{① moves out,} \\ & \text{② will not necessary} \end{cases}$

$\rightarrow$ | d.o.f = 6 |

(the two atoms are <u>completely independent</u>)

$\rightarrow$ | Ave KE per monoatomic molecule: $\frac{3}{2}kT$ |

Thermal Behavior of Matter (Cont.)

When heat is supplied to matter what are the consequences?
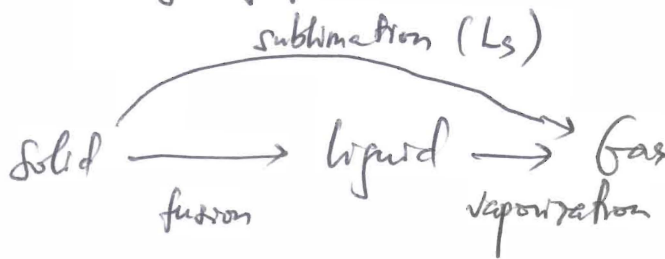
$\downarrow$

ΔQ

1) Temperature increase: $\Delta T \rightarrow \Delta Q = mc \Delta T$ (Ch 16)

2) Expansion
   $\begin{cases} \text{Linear expansion coefficient}: \alpha = \dfrac{\frac{\Delta L}{L}}{\Delta T} \\ (\text{Length} = L; \text{ temp} = T) \\[2em] \text{volume expansion coefficient}: \beta = \dfrac{\frac{\Delta V}{V}}{\Delta T} \\ (\text{Volume} = V, \text{ temp} = T) \end{cases}$

3) Change of phase :

   $\Delta Q = m L$

   $\qquad \downarrow \quad \downarrow$

   mass latent heat

   L_s, L_f, L_v

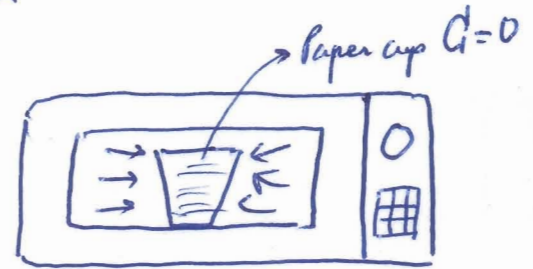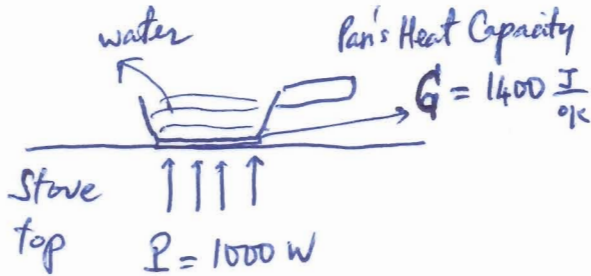   Different depending on the particular change of phase

Solid $\xrightarrow{\text{fusion}}$ liquid $\xrightarrow{\text{vaporization}}$ Gas

sublimation (L_s) (arrow from Solid to Gas)

Table 17.1

water $\begin{cases} L_f = 334 \ \dfrac{kJ}{kg} \\ L_v = 2257 \ \dfrac{kJ}{kg} \end{cases}$

16.49/

1) Write down data & making a sketch

2) Write down the appropriate equation

3) Solve for needed information

1)

water   Pan's Heat Capacity

$G = 1400 \frac{J}{°K}$

Stove top $P = 1000 W$

Paper cup $G = 0$

Microwave $P = 625 W$

Heat Capacity: $G = c \cdot m$

specific heat   mass

Relating to the expression for heat exchange:

$$\Delta Q = mc\,\Delta T = G\,\Delta T$$

a) Question: How much water before it is [faster] to heat using the stove top?

→ Start with an amount of water of mass m

→ Find how long it would take to increase the temperature by ΔT using stove Δt_S and using the microwave: Δt_M and then set $\Delta t_S < \Delta t_M$ → find that critical mass

2)(3)

Stove

Microwave

Δt_m

$\Delta t_s \leftarrow$ time to heat m_w so its temperature rises ΔT

$H_s = 1000\,W = \dfrac{\Delta Q}{\Delta t_s}$

$H_m = 625\,W = \dfrac{\Delta Q}{\Delta t_m}$

$\Delta t_s = \sqrt{\dfrac{\Delta Q}{1000}} = \dfrac{(C_w + C_{pan})\Delta T}{1000}$

$\Delta t_m = \dfrac{\Delta Q}{625} = \dfrac{(C_w + 0)\Delta T}{625}$ ← paper cup

Heat supplied by stove top is absorbed by both water & pan

Heat supplied by the microwave is absorbed only by water (paper cup's heat capacity $C \approx 0$)

$C_w = 4184\,\dfrac{J}{kg\,\cdot K}$; $C_{pan} = 1400\,\dfrac{J}{{}^\circ K}$

We need mass of water: m_w

$\rightarrow C_w = m_w C_w$

$\Delta t_s = \dfrac{(m_w 4184 + 1400)\cdot \Delta T}{1000}$

$\Delta t_m = \dfrac{(m_w 4184)\Delta T}{625}$

3) When is it faster to heat m_w with stove?

$$\Delta t_s < \Delta t_m$$

$$\dfrac{(m_w 4184 + 1400)\Delta T}{1000} < \dfrac{m_w 4184\,\Delta T}{625}$$

$$1.4 < m_w\left(\dfrac{4184}{625} - \dfrac{4184}{1000}\right)$$

$$\underbrace{\qquad\qquad}_{4184 \times 0.375}$$

$$\dfrac{1.4}{4184 \cdot 0.375} < m_w \qquad \text{or} \qquad \boxed{0.558\,kg < m_w}$$

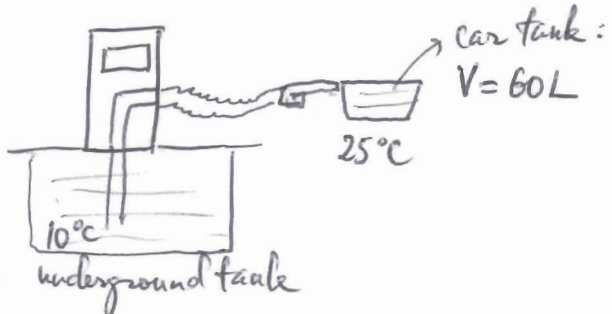5) What is the rate at which the temperature of this much water rises? $\dfrac{\Delta T}{\Delta t}$ $m_w = 0.558\,kg$.

$$\Delta t_s = \frac{(C_w + C_{pan})\Delta T}{1000} \rightarrow \frac{1000}{C_w + C_{pan}} = \frac{\Delta T}{\Delta t_s}$$

$$\rightarrow \frac{\Delta T}{\Delta t_s} = \frac{1000}{0.558 \cdot 4184 + 1400} = 0.268\,\frac{°K}{s}$$

17.63

1)

car tank:
$V = 60L$

25°C

10°C
underground tank

2) Coefficient of volume expansion $\beta \equiv \dfrac{\frac{\Delta V}{V}}{\boxed{\Delta T}}$

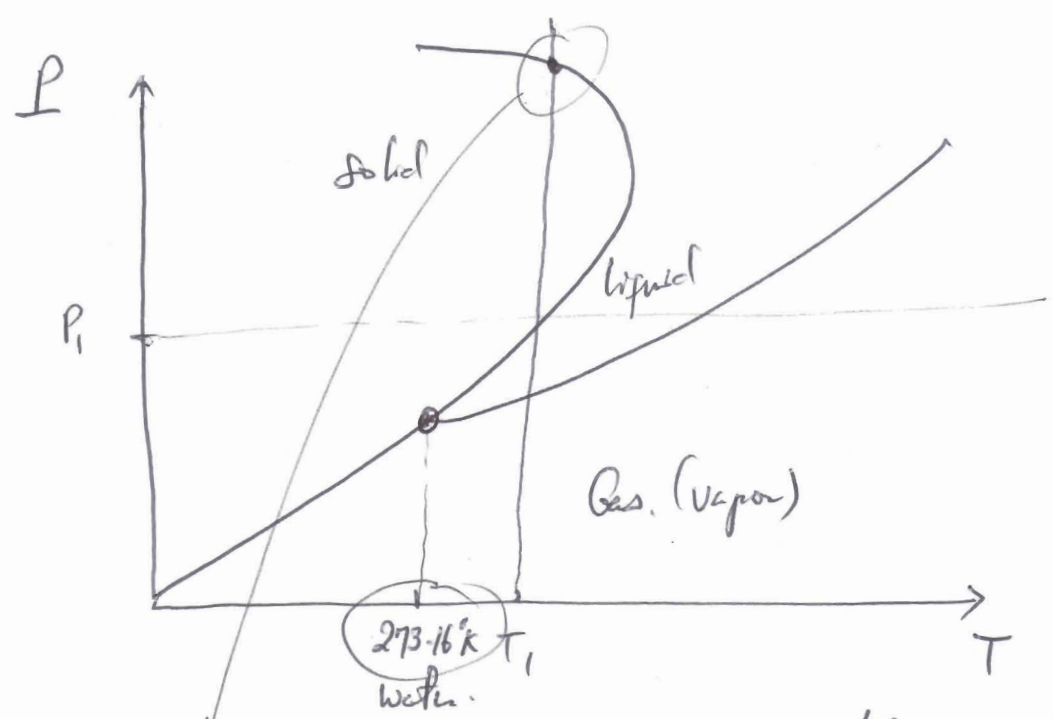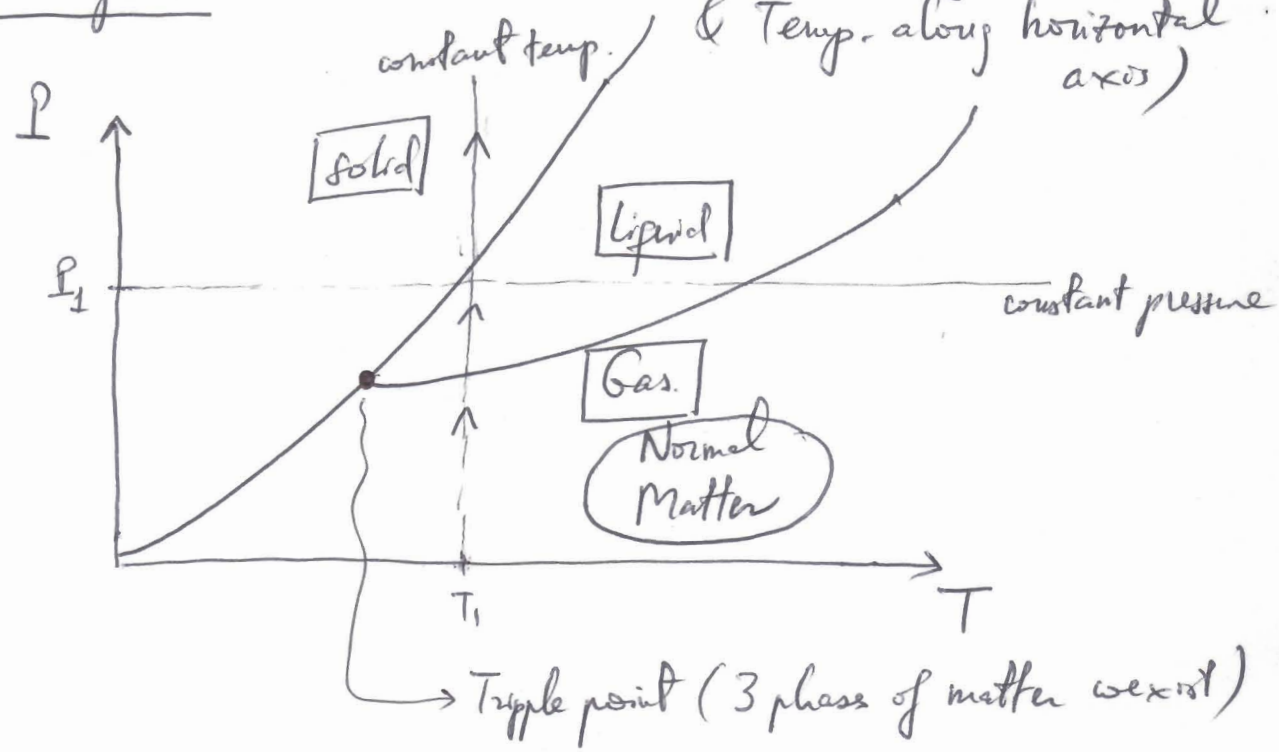$$\beta \Delta T = \frac{\Delta V}{V} \rightarrow \Delta V = \beta \Delta T V$$

↓ additional volume by thermal expansion

/ original volume of gasoline or the volume we can pump in

$$60 = V + \Delta V = V + \beta \Delta T V = V(1 + \beta \Delta T)$$

$$\boxed{V = \frac{60L}{1 + \beta \Delta T}} = \frac{60L}{1 + 95\times10^{-5}\times15} = \boxed{59.2\,L}$$

$°C$ or $°K$

$\beta_{Gasoline}$ (data) $= 95 \times 10^{-5}\,°K^{-1}$; $\Delta T = T_H - T_c \doteq 15\,°K$

Phase Diagram :   P vs. T   (Pressure along vertical axis
                                 & Temp. along horizontal
                                         axis)

constant temp.

P

P_1 ──────── constant pressure

solid

Liquid

Gas.

Normal
Matter

T_1

→ Tripple point (3 phases of matter coexist)

P

solid

liquid

P_1

Gas. (vapor)

(273·16 k) T_1

Water.

→ Water anomaly { If we increase pressure here, solid goes into liquid !

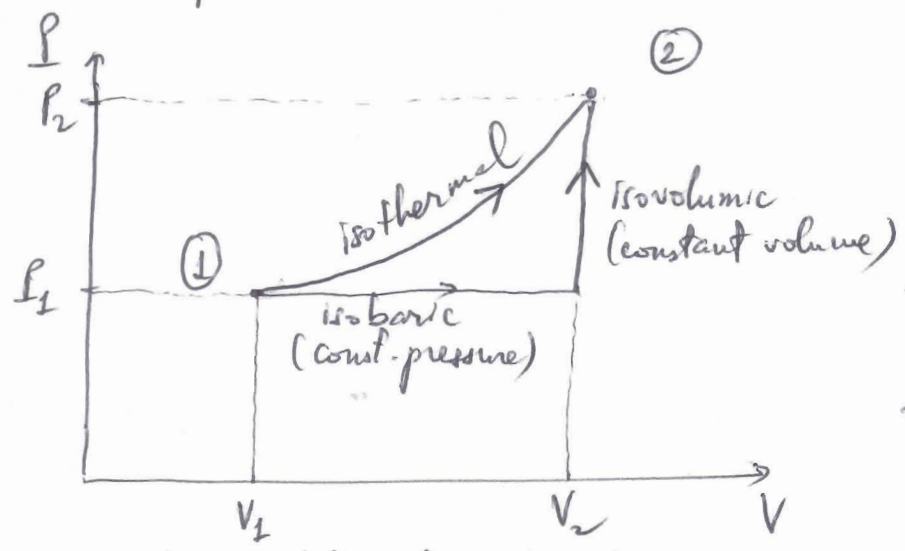# Ch 18   Heat, Work, 1st Law of Thermodynamics

1st Law of Thermodynamics:

$$\boxed{\Delta U} = \widehat{Q} - W$$

(Conservation of energy)

→ State Variable

Not state variables

ΔU: change of internal energy of a system

Q: heat absorbed by system

W: work done by system.

A state is a point on a PV diagram (P along vertical axis, V along horizontal axis). ΔU is a state variable since given a state ΔU is determined uniquely. Now $Q \& W$ are not state variables, they depend on a particular process b/w states!

Two alternative way to ① → ②

1) Via an isothermal process (fixed T)

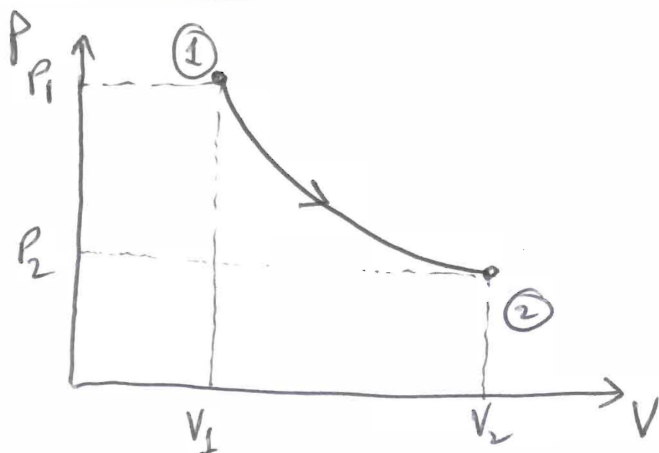2) Isobaric + Isovolumic processes

Process: connects 2 different states.

ΔU_{12}: change of internal energy of a system b/w ① & ②. It is unique regardless of which process it followed b/w ① & ②

$Q \& W$ b/w ① & ② depend on whether it ~~these~~ followed isothermal or isobaric + isovolumic processes.

→ Work done by a system: $W = \int P\, dV$

Quick check: $W = F \cdot \Delta x = \dfrac{P \cdot A \cdot \Delta x}{\Delta V}$

↓ force applied   ↘ displacement

Pressure $P = \dfrac{F}{A}$

Area under the curve in a PV diagram
is $W = \int P\, dV$

Process:
1) Isothermal   (T is constant)
2) Isovolumic   (V is constant)
3) Isobaric   (P is constant)
4) Adiabatic   (No heat absorbed or Q=0)

↳ Q & W depends on a particular process !

(ideal gas)

Isothermal (T is fixed)

$$V_2 > V_1 \\ P_2 < P_1 \;\Big\} \; \text{Isothermal expansion}$$

$$\to \quad W = \int_1^2 P\,dV = nRT \int_1^2 \frac{dV}{V} = nRT \left[\ln V\right]_1^2 = nRT\left(\ln V_2 - \ln V_1\right)$$

$$\underbrace{\qquad}_{\ln\left(\frac{V_2}{V_1}\right)}$$

ideal gas: $PV = nRT$

$\underbrace{}$ This is constant!
(isothermal)

$$\to P = \frac{nRT}{V}$$

$$\boxed{W = nRT \ln\left(\frac{V_2}{V_1}\right)} \quad \text{(work done by an ideal gas in an isothermal process)}$$

$$\to \quad Q = \Delta U + W \qquad \to \quad \underline{\text{What is } \Delta U \text{ in an isothermal process for ideal gases?}}$$

1st Law $\Delta U = Q - W$

Ideal gas:

1) No interactions b/w molecules $\longleftrightarrow$ no potential energy
   $\longleftrightarrow$ total internal energy of gas comes from kinetic energy only

2) Average KE per molecule in an ideal gas is $\begin{cases} \frac{3}{2} kT & \text{monoatomic molecules} \\ \frac{5}{2} kT & \text{diatomic molecules.} \end{cases}$
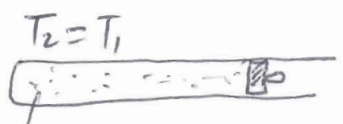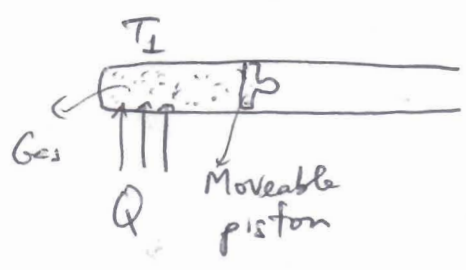
$\Delta U = 0$
for isothermal process

3) $\Delta U_{12} = U_2 - U_1 = \begin{cases} \frac{3}{2} k(T_2 - T_1) N = 0 \\ \frac{5}{2} k(T_2 - T_1) N = 0 \end{cases} \begin{array}{l} \text{Isothermal} \\ \text{process b/w ① & ②} \\ T_2 = T_1 \end{array}$

$$\to \boxed{Q = W} \; \text{ in isothermal process (ideal gas)}$$

Gas piston expansion:

T_1

Gas

Q Moveable piston
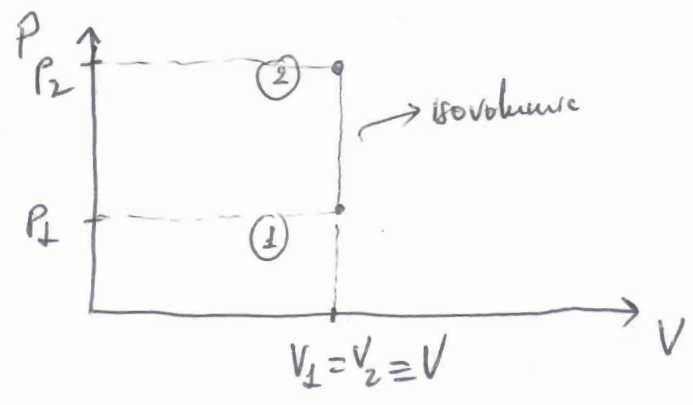
$T_2 = T_1$

Gas Isothermal expansion

Work done by piston $W = Q$

(since $\Delta U = 0$ for isothermal process
for ideal gas)

Isovolumic (Constant V)

$$W = \int_1^2 P \, dV = 0$$

$$Q = \Delta U$$ → What is ΔU in isovolumic process in ideal gas?
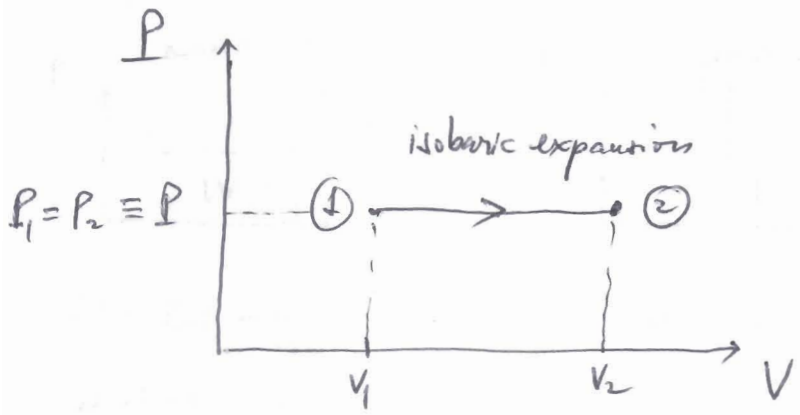
1st Law: $\Delta U = Q - W$

↳ c_v = specific heat at constant volume

$$c_v \equiv \frac{1}{n} \frac{Q}{\Delta T} = \frac{1}{n} \frac{\Delta U}{\Delta T}$$

moles

$$Q = c_v n \Delta T = \Delta U$$

Isobaric Process (Const. Pressure):

$$\boxed{W = \int_1^2 P \, dV = P \int_1^2 dV = P \underbrace{(V_2 - V_1)}_{\Delta V} = P \cdot \Delta V}$$

↓
Valid for any gas
(we did not use
ideal gas equation!)

$Q = ?$

$c_p =$ specific heat @ const pressure : $c_p = \dfrac{1}{n} \dfrac{Q}{\Delta T}$

$$\boxed{Q = n \, c_p \, \Delta T}$$

Ideal gas: $\qquad P \Delta V = n R \Delta T$

1st Law of T.D: $\Delta U = Q - W$

$n c_v \Delta T \qquad n c_p \Delta T \qquad P \cdot \Delta V = n R \Delta T \rightarrow \boxed{C_v = C_p - R}$
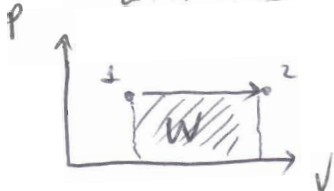
or $\boxed{C_p = C_v + R}$

$R = 8.314 \dfrac{J}{mol \, °K}$

There is more heat absorption
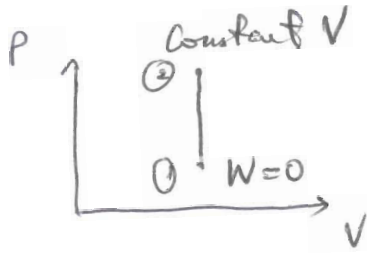capacity @ constant pressure than
@ constant volume

$$C_p = C_v + R$$

constant P

$$Q = \Delta u + \boxed{W}$$

If it can do work
it can keep absorbing
heat !

Constant V

$$Q = \Delta u$$

Adiabatic Process $(Q = 0)$

1st Law of T.D. : $Q = \Delta u + W$

$$\boxed{W = -\Delta u}$$

adiabatic
expansion

$$W = \frac{P_1 V_1 - P_2 V_2}{\gamma - 1}$$

$\hookrightarrow$ dimensionless coefficient $\gamma \equiv \dfrac{C_p}{C_v}$

Since C_v take on different values depending on the type of gas :

monoatomic $C_v = \dfrac{1}{n} \dfrac{N \frac{3}{2} k \Delta T}{\Delta T} = \dfrac{3}{2} k \dfrac{N}{\frac{n}{N_A}} = \dfrac{3}{2} k N_A = \dfrac{3}{2} R$

$$C_v = \frac{1}{n} \frac{\Delta u}{\Delta T} = \begin{cases} \\ \\ \end{cases}$$

diatomic $C_p = \dfrac{5}{2} R$

$$\gamma = \frac{C_P}{C_V} = \frac{C_V + R}{C_V}$$

$$\begin{cases} \text{Monoatomic} \quad \gamma = \dfrac{\frac{3}{2}R + R}{\frac{3}{2}R} = \dfrac{5}{3} = 1.67 \\[4mm] \text{Diatomic} \quad \gamma = \dfrac{\frac{5}{2}R + R}{\frac{5}{2}R} = \dfrac{7}{5} = 1.4 \end{cases}$$

<u>Adiabatic Process:</u>

$$\boxed{P_1 V_1^{\gamma} = P_2 V_2^{\gamma}}$$

ideal gas: $PV = nRT$ or $P = \dfrac{nRT}{V}$ $\Big\} \rightarrow$ $\boxed{T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1}}$

16.75

$$\begin{cases} m_w = 5.4 \times 10^6 \, kg \\ \Delta T = 350°C - 10°C = 340 °K \end{cases}$$ (water remains liquid → no change of phase : no vaporization)

Thermal power output $P = 1.42 \times 10^9 \, W$

<u>How long</u> would it take to heat m_w from $10°C$ to $350°$?

$\Delta t? \quad$ 1) Total energy needed : $\Delta Q = m_w \, c_w \, \Delta T = 5.4 \times 10^6 \times 4184 \times 340 \, J$

2) Use heat transfer rate to find $\Delta t = \dfrac{\Delta Q}{P} = \dfrac{5.4 \times 10^6 \times 4184 \times 340}{1.42 \times 10^9}$

$$= 5400 s = 1.5 \, hrs.$$

18.33

Air bubble in blood $\begin{cases} \quad \end{cases}$

$d_L = 1.52 mm \quad @ \; P_L = 80 \, mm \, Hg$

$d_H \; ? \qquad @ \; P_H = 125 \, mm \, Hg$

Notes :
- These values for P_L & P_H are gauge pressures (excesses above the atmospheric pressure : $760 \, mm \, Hg$ or $1 \, atm$)
- We expect air bubble to be smaller ($d_H < d_L$) when blood pressure is @ P_H

a) Body temp. is constant @ $37°C$ → so will be the air temp. inside bubble : → assume it's an ideal gas $\begin{cases} P_L V_L = nRT \\ P_H V_H = nRT \end{cases} \boxed{P_L V_L = P_H V_H}$

$\quad \hookrightarrow V_H = \dfrac{P_L V_L}{P_H} \qquad ; \quad$ volume of sphere in term of its diameter :

$$\boxed{V = \tfrac{4}{3} \pi \left(\tfrac{d}{2}\right)^3 = \tfrac{\pi}{6} d^3}$$

$\downarrow$

$\dfrac{\pi}{6} d_H^3 = \dfrac{(80 + 760) \, \tfrac{\pi}{6} d_L^3}{(125 + 760)} \qquad ;$ Note : mm of Hg to Pa (Pascal, SI unit for Pressure) is only scaling factor that will cancel up & down in the fraction $\dfrac{P_L}{P_H}$

To solve for d_H : elevate both sides to the power of $\frac{1}{3}$

$$d_H = \left(\frac{840}{885}\right)^{\frac{1}{3}} d_L = \left(\frac{840}{885}\right)^{1/3} 1.52\,mm = 1.49^{38}\,mm$$

(Note: $d_H < d_L$ as expected)

b)
Work $\begin{cases} \text{– As the bubble compresses (by 0.03 mm) the blood \& heart have done some work! this work is received by gas inside bubble.} \\ \text{– Gas undergoes an isothermal process } ① → ② \text{ or } \underset{P_L, V_L}{Ⓛ} → \underset{P_H, V_H}{Ⓗ} \end{cases}$

$$W = nRT \ln\left(\frac{V_2}{V_1}\right) = P_L V_L \ln\frac{V_H}{V_L}$$

$\downarrow$
work done by
gas
$\downarrow$

$$= 840 \cdot \underbrace{\frac{1.013\times10^5}{760}}_{P_L} \cdot \underbrace{\frac{4\pi}{3}\left(\frac{1.52\times10^{-3}}{2}\right)^3}_{V_L} \cdot \underbrace{\ln\left[\frac{(1.49)^3}{(1.52)^3}\right]}_{\ln\left(\frac{V_H}{V_L}\right)}$$

Work done by
heart is $-W$

$$= -12.3\times10^{-6}\,J = -12.3\,\mu J \quad ? \quad (-10.7\,\mu J)$$

if using
$d_H = 1.4938\,mm$

$\begin{cases} 1\,Atm = 1.013\times10^5\,Pa \\ \text{same as } 760\,mm\,Hg. \end{cases}$ $P_L = 840\,\cancel{mm\,Hg} \cdot \dfrac{1.013\times10^5\,Pa}{760\,\cancel{mm\,Hg}}$

$$10^{-6} = micro = \mu$$

Note : Work done by gas in going Ⓛ → Ⓗ is negative
since it was compressed in this process ($V_H < V_L$)
so it received work.
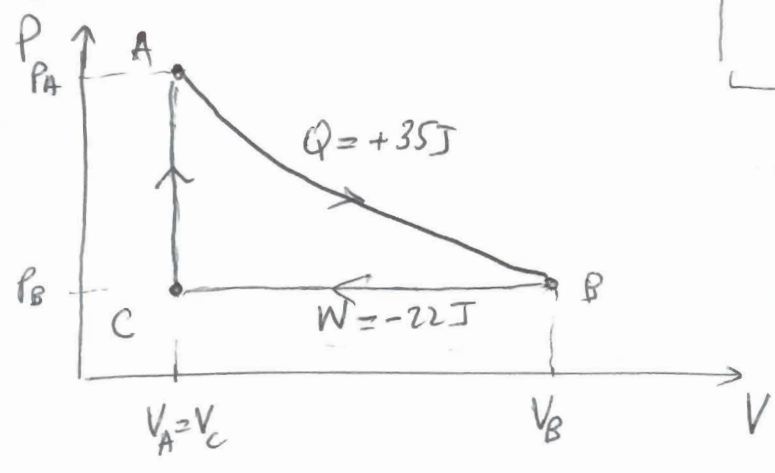Work done by heart is $-W = \boxed{+12.3\,\mu J}$

18.42

a)

Gas:

undergoes a cycle

$$\underset{\substack{\text{isothermal} \\ \text{exp}}}{A \longrightarrow} \underset{\substack{\text{isobaric} \\ \text{comp}}}{B \longrightarrow} C$$
$$\underset{\text{isovolumic}}{\curvearrowleft}$$

isothermal expansion always comes with a decrease in pressure: $PV = nRT$ = const.

$A \rightarrow B$ gas absorbs heat Q is positive!

$B \rightarrow C$: isobaric @ P_B
$V_C = V_A$
Work done on gas $\approx 22 J$
$W =$ is work done by gas $W = -22 J$

$C \rightarrow A$: isovolumic

b) How much ⟨work⟩ is done on or by gas during complete cycle?

depends on the process

$$A \rightarrow B \rightarrow C \rightarrow A$$
$$\downarrow \qquad \downarrow \qquad \qquad \downarrow$$
$$W_{AB} \quad W_{BC} = -22J \quad W_{CA} = 0 \text{ (Isovolumic)}$$

$$\left. \right\} \; W_{ABCA} = W_{AB} + W_{BC}$$
$$\underset{?}{\phantom{W_{AB}}} \qquad \underset{-22J}{\underbrace{\phantom{W_{BC}}}}$$

W_{AB}: 1st Law: $\Delta U_{AB} = Q_{AB} - W_{AB}$
$\downarrow$

Ideal gas $T_A = T_B$
$\downarrow$
$U = \frac{1}{2}mv^2$
$= \frac{3}{2}kT$ $0 = 35J - W_{AB}$

$\rightarrow \boxed{W_{AB} = 35J}$

$$W_{ABCA} = 35J - 22J = \boxed{(+) 13J}$$
$$\downarrow$$
$$\text{Work done by gas.}$$

c) How much heat is transferred to or from gas

$B \rightarrow C \rightarrow A$
$\downarrow \qquad \downarrow$
isobaric isovolumic

$$Q_{BCA} = Q_{ABCA} - Q_{AB}$$

Q_{ABCA} ? 1st Law of TD : $\Delta U_{ABCA} = Q_{ABCA} - W_{ABCA}$

$$0 = Q_{ABCA} - 13 J$$

$Q_{ABCA} = 13 J$

$Q_{BCA} = 13 J - Q_{AB} = -22 J :$

$\quad\quad\quad\quad\quad\quad\underbrace{\quad}_{35 J}$

└→ Heat absorbed is negative → gas lost 22 J of heat during B→C→A.

Ch 19.   2nd Law of Thermodynamics

Heat engines working b/w 2 different reservoirs

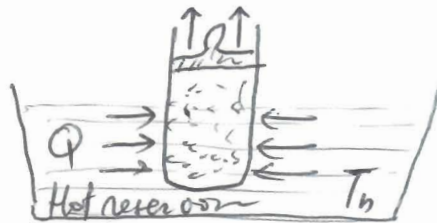<u>Heat reservoir</u> :   source of heat, large, at constant temperature

<u>Visual experiment</u> :   place a piston filled with ideal gas in thermal contact with a heat reservoir (hot) at temperature T_h. Gas absorbs heat, expands, does work. Alsen it absorbs heat, its temperature will increase. When its temperature reaches T_h : stops heat absorption, stops expansion, stops doing work. How do you make this into a heat engine or for the gas to continue doing work?

1) Keep raising the temperature T_h : not practical

2) Cooling it down to a lower temperature T_c (placing it in thermal contact with a cold reservoir) before placing it in contact again with the hot reservoir. Then repeat the cycle. Gas needs to receive work as it compresses while cooling, our goal is to get a net work done per cycle.
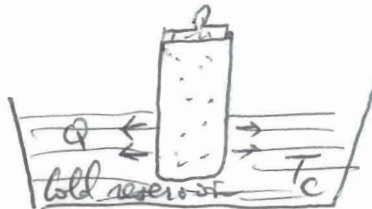
<u>Diagrams</u> :
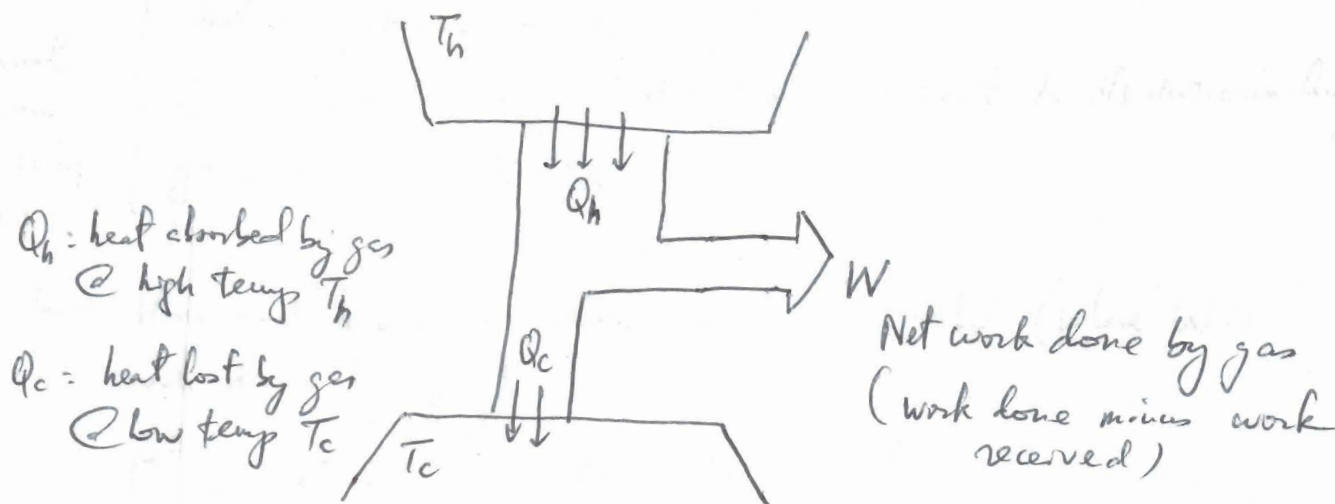
Cycle
$\Big\{$
1st half

Gas absorbs heat, does work

2nd half

Gas ejecting heat, receives work.

$\boxed{\text{Heat engine}}$ in one diagram:

Q_h: heat absorbed by gas
@ high temp T_h

Q_c: heat lost by gas
@ low temp T_c

W
Net work done by gas
(work done minus work received)

1st law of T.D. on a heat engine:

$$\underbrace{\Delta U}_{0} = Q_{net} - W = \underbrace{Q_h - Q_c}_{Q_{net}} - W = 0$$

After one cycle:
(back to its initial state)

$\boxed{Q_h - Q_c = W}$ → Net heat absorbed is net work done

Efficiency of a heat engine: $e = \dfrac{W}{Q_h} = \dfrac{Q_h - Q_c}{Q_h} = 1 - \dfrac{Q_c}{Q_h}$

↳ $e = 1 - \underbrace{\dfrac{|Q_c|}{|Q_h|}}_{} < 1$

↳ Absolute values are to ensure $e < 1$ b/c:

2nd Law of T.D.: it is impossible to build a heat engine operating in cycles that extracts heat from a hot reservoir and returning some of it to a cold reservoir, that can deliver 100 % efficiency ($e = 1$ is not possible! → $e < 1$)

(18.52)

External forces were compressing a gas.

$$\begin{cases} n = 21 \\ \text{ideal monoatomic} \rightarrow C_V = \frac{3}{2}R \\ Q = -15\,kJ \quad (\text{gas lost } 15kJ \text{ of heat to its surroundings}) \\ \Delta T = T_f - T_i = 160\,°K \end{cases}$$

↳ How much work was done on gas? $-W$ (where W is work done by gas)

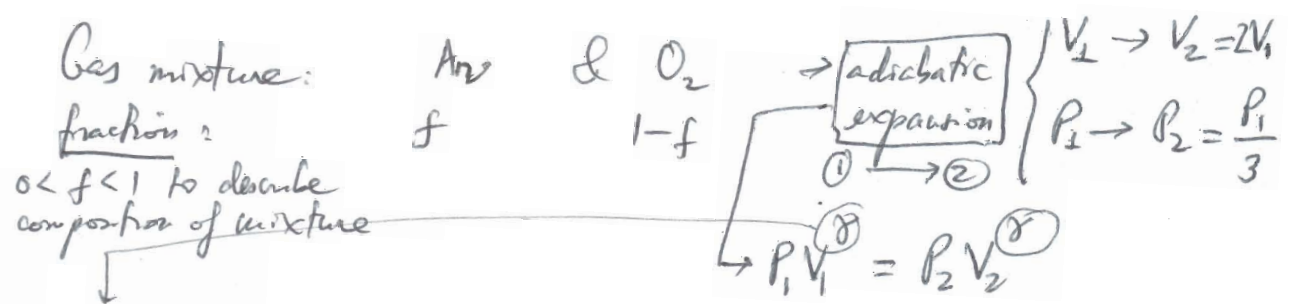1st law of T.D: $\quad \Delta U = Q - W$

Change of internal energy of gas → heat absorbed by gas → Work done by gas.

$$\rightarrow \quad -W = \Delta U - Q$$

$$= n\,C_V\,\Delta T - Q$$

$$= 21 \times \frac{3}{2} \times 8.314^{\times 160} - (-15000)$$

$$= 56900\,J$$

→ Work done on gas is $+56.9\,kJ$

(18.57)

Gas mixture:

	Air	& O_2
fraction:	f	$1-f$

$0 < f < 1$ to describe composition of mixture

→ adiabatic expansion

$$\begin{cases} V_1 \rightarrow V_2 = 2V_1 \\ P_1 \rightarrow P_2 = \frac{P_1}{3} \end{cases}$$

① → ②

$$\hookrightarrow P_1 V_1^{\gamma} = P_2 V_2^{\gamma}$$

$$\gamma = \frac{C_p}{C_v}$$

$\underbrace{\gamma, C_p, C_v}$ are for the mixture

↳ Strategy: 1) f will appear in expression of γ for the mixture
2) Find value of γ from adiab. expansion → find f

Mixture: $c_v = \dfrac{3}{2}R\,f + \dfrac{5}{2}R\,(1-f)$

$\underbrace{\qquad}_{\substack{monoatomic \\ A_r}} \qquad \underbrace{\qquad}_{\substack{diatomic \\ O_2}}$

$$\gamma = \frac{c_p}{c_v} = \frac{c_v + R}{c_v} = \frac{\frac{3}{2}Rf + \frac{5}{2}R(1-f) + R}{\frac{3}{2}Rf + \frac{5}{2}R(1-f)}$$

$$\gamma = \frac{\frac{7}{2} - f}{\frac{5}{2} - f}$$

Adiabatic expansion: $\quad P_1 V_1^{\gamma} = P_2 V_2^{\gamma} \rightarrow \dfrac{P_1}{P_2} = \left(\dfrac{V_2}{V_1}\right)^{\gamma}$

$$\ln\left(\frac{P_1}{P_2}\right) = \gamma \ln \frac{V_2}{V_1}$$

$$\gamma = \frac{\ln\left(\frac{P_1}{P_2}\right)}{\ln\left(\frac{V_2}{V_1}\right)} = \frac{\ln 3}{\ln 2}$$

$$\gamma = 1.58$$

$\gamma = 1.58 = \dfrac{\frac{7}{2} - f}{\boxed{\frac{5}{2} - f}} \quad \rightarrow \quad \dfrac{5}{2}\gamma - \gamma f = \dfrac{7}{2} - f$

$$\frac{5}{2}\gamma - \frac{7}{2} = (\gamma - 1) f$$

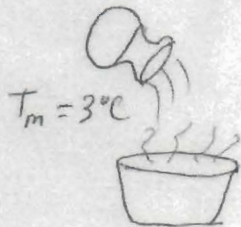$$\rightarrow f = \frac{\frac{5}{2}\gamma - \frac{7}{2}}{\gamma - 1}$$

$$= \frac{\frac{5}{2}\cdot 1.58 - \frac{7}{2}}{0.58}$$

$$\boxed{f = 0.78}\ \ A_r$$

$$\boxed{\begin{array}{l} A_r = 78\% \\ O_2 = 22\% \end{array}} \quad \longleftarrow$$

(16-54)

milk $m_m = 2 oz$

$T_m = 3°C$

cocoa

$T_c = 90°C$

$m_c = 6 oz$

milk & cocoa @ T_f?

$C_m = C_c = C_{water} = 4184 \dfrac{J}{kg \, °k}$

Heat balance equation: $\Delta Q_c + \Delta Q_m = 0$
(isolated system)

$$m_c C_c (T_f - T_c) + m_m C_m (T_f - T_m) = 0$$
$$\underbrace{}_{C_w} \qquad\qquad \underbrace{}_{C_w}$$

$$(m_c C_w + m_m C_w) T_f = m_c C_w T_c + m_m C_w T_m$$

$$T_f = \frac{m_c T_c + m_m T_m}{m_c + m_m}$$

$SI \begin{cases} T \to in \, °k \to T_c = 90° + 273.16° \\ \qquad = 363.16 \, °k \\[4pt] T_m = 3° + 273.16° \\ \qquad = 276.16 °K \\[4pt] m \to in \, kg \text{ (not necessary in this particular eq.)} \end{cases}$

masses showing above & below the fraction!

$$T_f = \frac{6 \times 363.16 + 2 \times 276.16}{8} = 341.46 \, °K$$

Can go back to celsius: $T_f = 341.46 - 273.16 = 68.3 °C$

If I work in celsius:

$$T_f = \frac{m_c (T_{c_K} - 273.16) + m_m (T_{m_K} - 273.16)}{m_c + m_m}$$

$$= \underbrace{\frac{m_c T_{c_K} + m_m T_{m_K}}{m_c + m_m}}_{T_{f_K}} + \frac{(m_c + m_m)(-273.16)}{(m_c + m_m)}$$

$$T_f = T_{f_K} - 273.16$$

(17.65)

Thermal resistance of fridge wall is $R = 0.12 \frac{°K}{W}$

Fridge: → ΔQ

Heat will come in through walls only delayed by [Thermal resistance R]

$$R \equiv \frac{\mathcal{R}}{A}$$ → R-factor

→ area

R → determine H (Heat transfer rate through fridge's walls)

→ how long will ice will last $\Delta t = \dfrac{\Delta Q}{H}$ $\left(H = \dfrac{\Delta Q}{\Delta t} \right)$

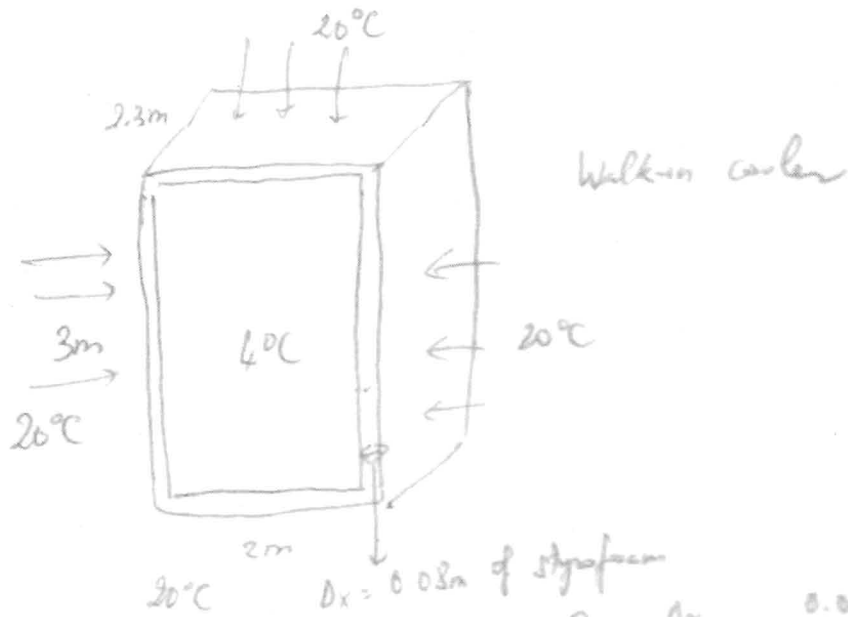ΔQ will go into melting the ice or $m_{ice} L_f$

$$H = -kA \frac{\Delta T}{\Delta x} = -\frac{A \Delta T}{\mathcal{R}} = -\frac{\cancel{A} \Delta T}{R \cancel{A}} = -\frac{\Delta T}{R}$$

(Heat transferred from outside to inside → $H_{absorbed} = \dfrac{\Delta T}{R}$)

$$\Delta t = \frac{\Delta Q}{H_{abs.}} = \frac{m_{ice} L_f}{\frac{\Delta T}{R}} = \frac{15 \times 334 \times 10^3}{\frac{(20-0)}{0.12}} = 3 \times 10^4 s \frac{1h}{3600s}$$

$$= 8.35 \, h$$

$L_f \,(\text{water}) = 334 \, \frac{kJ}{kg}$

16.56

20°C

2.3m

Walk-in cooler

3m

4°C

20°C

20°C

2m

20°C $\Delta x = 0.08m$ of styrofoam

$$H = -\frac{A\Delta T}{R}$$

$$R = \frac{\Delta x}{k} = \frac{0.08}{0.029} = 2.76$$

Table 16-2

$$A = \underbrace{3 \times 2 \times 2}_{\text{Front & Back}} + \underbrace{3 \times 2.3 \times 2}_{\text{Left & right}} + \underbrace{2.3 \times 2 \times 2}_{\text{Top & bottom}}$$

$$= 35m^2$$

$$\boxed{H = -\frac{32 \times 16}{2.76} = -203 \, W}$$

(17.71) Clock   brass pendulums: $L = 0.2\,m$ @ $20°C$ (good)
(calibrated to work as a clock @ $20°C$.

$\downarrow$

$T_2 = 13°C \longrightarrow$ how long until it makes a 1min error?

Since for a pendulum: # oscillations per second $\omega = \sqrt{\dfrac{g}{L}}$

length will change with temp, according to the linear coefficient
of expansion for brass: $\rightarrow$ Table 17.2 : $\alpha = 19 \times 10^{-6}\,°K^{-1}$

$$\alpha = \frac{\frac{\Delta L}{L}}{\Delta T} \rightarrow \frac{\Delta L}{L} = \alpha \Delta T \rightarrow \Delta L = \alpha L \Delta T$$

$$T = \frac{2\pi}{\omega} = 2\pi \sqrt{\frac{L}{g}} \quad \Bigg| \quad T_{20°c} = 2\pi \sqrt{\frac{L}{g}}$$

$$-2°K$$

$$T_{18°c} = 2\pi \sqrt{\frac{L + \Delta L}{g}} = 2\pi \sqrt{\frac{L + \alpha L \Delta T}{g}}$$

$$= 2\pi \sqrt{\frac{L(1 + \alpha \Delta T)}{g}}$$

$$T_{18°c} < T_{20°c} \rightarrow T_{20°c} - T_{18°c} = \frac{2\pi}{\sqrt{g}}\left[\sqrt{L} - \sqrt{L(1 + \alpha \Delta T)} \right]$$

$$= 2\pi \sqrt{\frac{L}{g}}\left[1 - \sqrt{1 - 2\alpha} \right]$$

$$\downarrow$$
$$\Delta T = -2°K.$$

$$\sqrt{1 - 2\alpha} = (1 - 2\alpha)^{1/2} \cong 1 - \frac{1}{2}(2\alpha) = 1 - \alpha$$

$$(1 + x)^{1/2} \simeq 1 + \frac{1}{2}x + \dots \uparrow$$

$\underbrace{\qquad\qquad}$
negligible if x very
small compared to 1

$$\alpha = 19 \times 10^{-6}\,°K^{-1}$$

$$\boxed{T_{20°} - T_{18°} = 2\pi \sqrt{\frac{L}{g}}\left[1 - (1 - \alpha) \right] = 2\pi \sqrt{\frac{L}{g}}\,\alpha} \quad \begin{array}{l}\text{time} \\ \text{error per period.}\end{array}$$

How many periods of pendulum until a difference of 1 min:

$$\frac{60s}{2\pi\sqrt{\frac{L}{g}}\,\alpha}$$

How long until a difference of 60s? $\quad\dfrac{60s}{2\pi\sqrt{\frac{L}{g}}\,\alpha}\, T_{20°}$

$$= \frac{60}{2\pi\sqrt{\frac{L}{g}}\,\alpha}\, 2\pi\sqrt{\frac{L}{g}}$$

$$= \frac{60}{\alpha} = \frac{60}{19\times10^{-6}}\,s \rightarrow \underline{\underline{36.5\,days}}$$

(17.39)

@ $T = 25°C$ (room temp.) $\rightarrow P = 180\,atm.$

a) How many moles of air n
   Assume ideal gas. $n = \dfrac{PV}{RT}$

$P = 180\,\cancel{atm}\cdot\dfrac{1.013\times10^5\,Pa}{1\,\cancel{atm}}$

$V = \pi(0.1)^2\cdot 1 = \dfrac{\pi}{100}\,m^3$

$R = 8.314\,\dfrac{J}{°K\,mol}$

$T = 25 + 273.16 = 298.16\,°K$

$$n = \frac{180\times1.013\times10^5\times\frac{\pi}{100}}{8.314\times298.16}$$

$$= 231\,mol$$

b) What would be the gas volume @ $P = 1\,atm$ & $T = 25°C$
   $\rightarrow n = 231 \quad \rightleftharpoons \quad \dfrac{PV}{RT}$ { if P decreases 180 fold
   $\rightarrow V$ increases 180 times

$$V = \frac{\pi}{100}\times180\,m^3 = 5.65\,m^3$$