

Ch16    Temperature & Heat

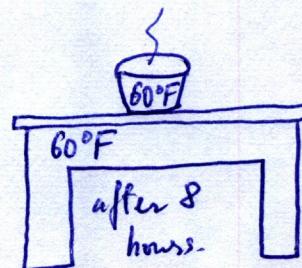
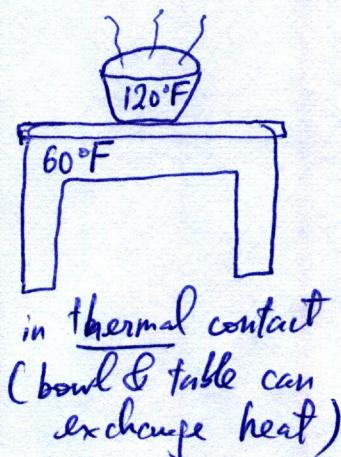
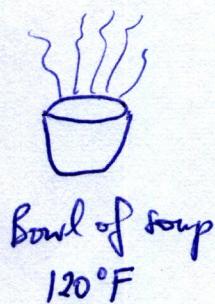
Temperature: a macroscopic property (we can sense & measure), it is a consequence of microscopic behavior of matter.

Unit:  $^{\circ}\text{F}$  (degree Fahrenheit)      SI:  $^{\circ}\text{K}$  (degree Kelvin) ( $\text{absolute zero is } 0^{\circ}\text{K}$ )  
 $^{\circ}\text{C}$   
(degree Celsius)

$$T_F = \frac{9}{5} T_C + 32 \rightarrow (\text{body temp. } \sim 100^{\circ}\text{F})$$

$$T_C = \frac{5}{9} (T_F - 32) \rightarrow (\text{boiling point of water } \sim 100^{\circ}\text{C})$$

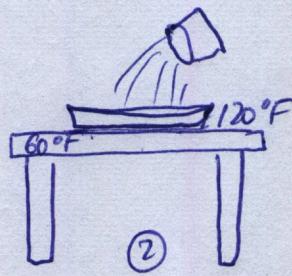
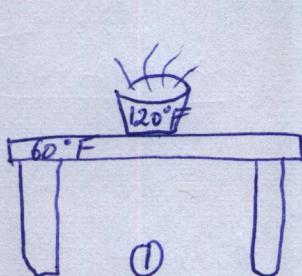
$$T_C = T_K - \underbrace{273.16\text{ }^{\circ}\text{K}}_{\text{Triple point of water}} \quad (3 \text{ phases coexist } @ \text{this temperature})$$



they have arrived at  
thermodynamic equilibrium  
(T.D.) or same temperature  
by exchanging heat

(2)

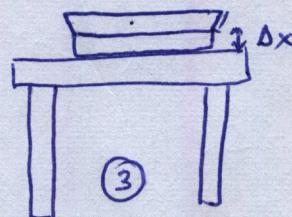
Heat transfer rate :  $H \rightarrow$  how fast heat can be transferred or exchanged b/w 2 objects.



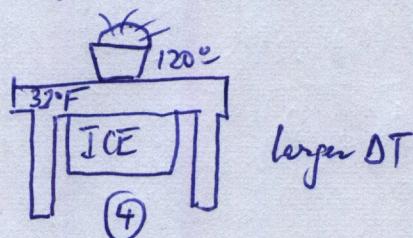
larger contact surface A

$$H = -k \frac{A}{\Delta x} \Delta T$$

Thermal constant  
(depending on materials)

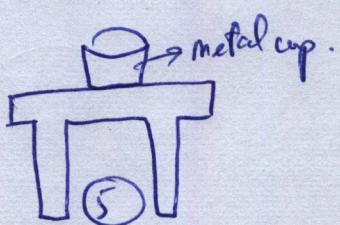


larger thickness  $\Delta x$



larger  $\Delta T$

① & ④ : Larger  $\Delta T \rightarrow$  faster heat transfer rate  $\rightarrow \uparrow H$



① & ⑤

faster transfer depending on material  
metal are faster heat conductors.

metal are also good electrical conductors

} free electrons  
↓  
energy carriers  
↓

"Temperature is a consequence of microscopic properties of matter"

(3)

<u>Units for <math>H</math>:</u>	SI	$\left\{ \begin{array}{l} \text{Length} \rightarrow L \rightarrow \text{meter (m)} \\ \text{Mass} \rightarrow M \rightarrow \text{kilogram (kg)} \\ \text{Temperature} \rightarrow T \rightarrow \text{degree Kelvin (°K)} \\ \text{Time} \rightarrow T \rightarrow \text{second (s)} \\ \text{Energy} \rightarrow M \frac{L^2}{T^2} \rightarrow \text{joule (J)} \\ \quad \downarrow \text{Mechanical (kinetic, potential)} \\ \quad \downarrow \text{Thermal or heat} \\ \text{Power} \rightarrow M \frac{L^2}{T^3} \rightarrow \text{joule/s = watt (W)} \end{array} \right.$

Dimension of  $H$ 

$$[H] = [k] [A] \frac{[\Delta T]}{[dx]} \rightarrow [k] = \frac{[E]}{[\text{Time}]} \frac{[dx]}{[\Delta T]} \frac{1}{[A]}$$

$$\downarrow \frac{[E]}{[\text{Time}]}$$

$$\text{Unit for } k: \frac{J}{s} \frac{\text{m}}{\text{°K}} \frac{1}{\text{m}^2} = \frac{W}{\text{m °K}}$$

$$K \rightarrow \left\{ \begin{array}{l} \text{SI: } \frac{W}{\text{m °K}} \\ \text{British: } \frac{\text{Btu} \cdot \text{in}}{\text{h ft}^2 \text{ °F}} \\ \quad \text{hour} \end{array} \right. \quad (\text{Btu : British thermal unit})$$

(Thermal constant)

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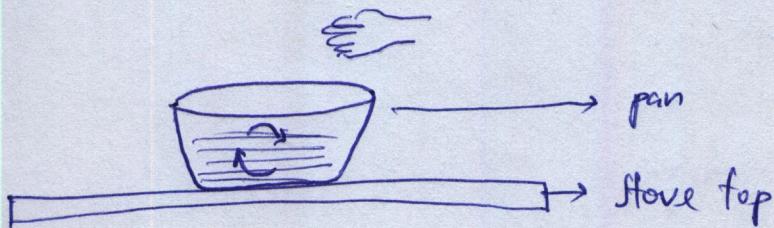
R-factor:  $R = \frac{dx}{k}$  (larger  $R$  better insulation)

$$H = - \frac{k A \Delta T}{dx} = - \frac{A \Delta T}{R}$$

Unit:  $\left\{ \begin{array}{l} \text{SI: } \frac{\text{m}^2 \text{ °K}}{\text{W}} \\ \text{British: } \frac{\text{ft}^2 \text{ °F}}{\text{Btu/h}} \end{array} \right.$

$\leftarrow R=21 \rightarrow R=21 \frac{\text{ft}^2 \text{ °F}}{\text{Btu/h}}$

## Mechanisms of heat transfer:



- Initially: stove top is heated.

Heat transfer: stove top  $\rightarrow$  pan by **conduction** (via free electrons in metal pan)

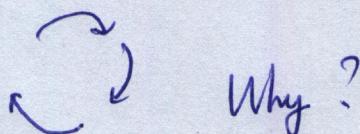
- Water at bottom gets heated

Heat transfer: bottom water  $\rightarrow$  top water by **convection** (circulation of water molecules)

→ Hand feels some heat

Heat transfer: hot water  $\rightarrow$  hand by **radiation** (does this require a medium  $\rightarrow$  No: we feel heat from sun!)  
 ↓  
 propagation of radiation via electromagnetic waves

### Convection:



Why?

hot molecules & atoms tend to stay apart  $\rightarrow$  lower density  
 $\rightarrow$  tend to rise above liquid or gases with higher density.  
 Reverse process for higher density  $\rightarrow$  tend to sink

### Radiation:

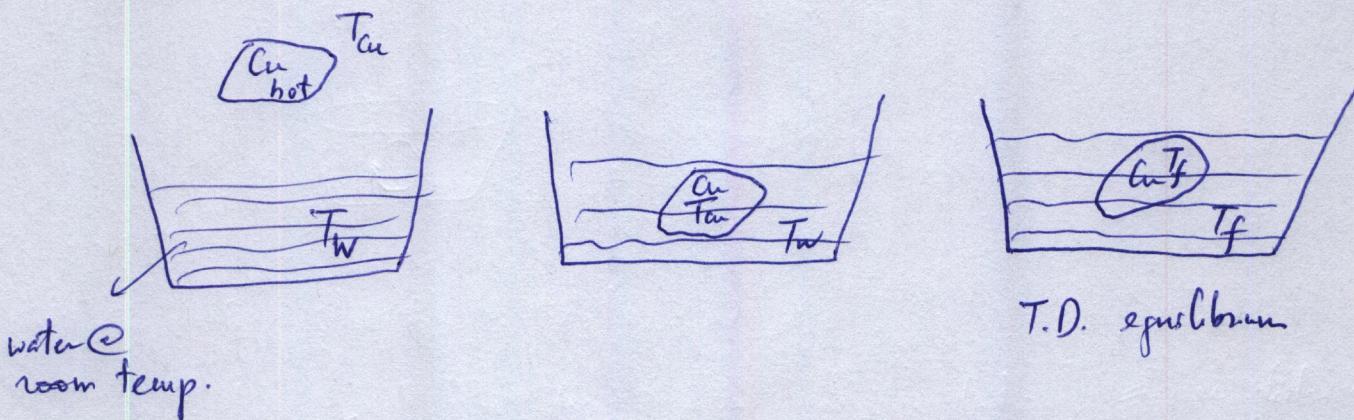
Stefan - Boltzmann Law: heat loss rate (per unit time) by radiation of an object of area A & temp. T:

$$P = e \downarrow \sigma \uparrow A T^4$$

emissivity (no unit)

$$\text{Stefan - Boltzmann constant} = 5.67 \times 10^{-8} \frac{\text{W}}{\text{m}^2 \text{K}^4}$$

## Heat balance equation :



Assume: system water (& bucket) & copper is isolated :

$$\underbrace{\Delta Q_{Cu}}_{\substack{\text{Heat loss} \\ \text{by Copper}}} + \underbrace{\Delta Q_W}_{\substack{\text{Heat gain} \\ \text{by water}}} = 0 \quad (\text{heat left copper went into water})$$

$$= m_{Cu} c_{Cu} (T_f - T_{Cu}) + m_W c_W (T_f - T_W) = 0$$

\underbrace{\qquad\qquad\qquad}\_{\substack{\text{specific heat} \\ \text{of Copper}}} + \underbrace{\qquad\qquad\qquad}\_{\substack{\text{water gets} \\ \text{heated}}}

Copper gets cooled down

$$\begin{cases} C_W = 4184 \frac{J}{kg \cdot K} \\ C_{Cu} = 386 \frac{J}{kg \cdot K} \end{cases}$$

Specific heat  
 ↓  
 Capacity to absorb heat per unit mass  
 Material-specific!

(6)

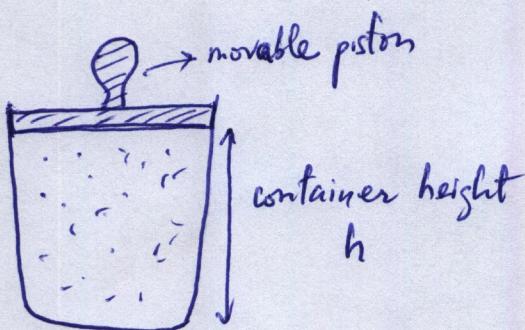
## Ch 17 Thermal Behavior of Matter

Matter : 3 states	Density	State
	low →	<u>Gas</u> : almost free molecules.
	Medium →	<u>Liquid</u> : not interacting some interaction b/w molecules

High → Solid : molecules are not free to move

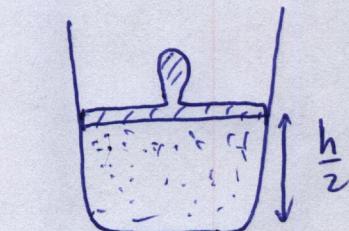
Gas → Ideal Gases : completely free (non-interacting) molecules.

- . Macroscopic quantities or properties:  $\{ T \text{ (temp., } ^\circ\text{K)} \\ P \text{ (pressure, Pa)} \\ V \text{ (volume, m}^3\text{)} \}$
- . Microscopic quantity :  $N$  (num. of molecules)



$T, N, V, P$

state ①



$T, N, \frac{V}{2}, 2P$

state ②

Assuming :

- Gas can't escape
- $① \rightarrow ②$  isothermal process (very slowly)

Equation of state for an ideal gas:

$$\begin{aligned} ① \rightarrow ② & \left\{ \begin{array}{l} N_1 T_1 = N_2 T_2 \\ P_1 V_1 = P_2 V_2 \end{array} \right. \end{aligned}$$

$$\Rightarrow P_1 V_1 = k N_1 T_1 \quad \& \quad P_2 V_2 = k N_2 T_2$$

PV = kNT

$$k = \text{Boltzmann constant} \rightarrow 1.38 \times 10^{-23} \frac{\text{J}}{\text{ok}}$$

(7)

Avogadro number :  $N_A = 6.022 \times 10^{23}$

$$N = n N_A ; \quad n: \text{number of moles}$$

$$\frac{PV}{N} = k \frac{n N_A}{N} T = n \frac{k N_A}{N} T \Rightarrow PV = nRT$$

$\boxed{R = 8.314 \frac{\text{J}}{\text{K mol}}}$

Ideal Gas

If we consider interactions b/w gas molecules  $\rightarrow$  Real Gas

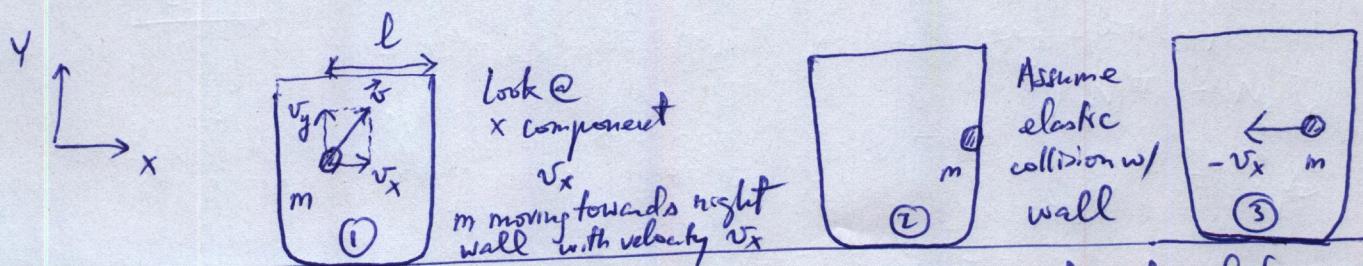
$\hookrightarrow$  Eq. of state for Real Gas or Van der Waals equation

$$\left( P + \frac{n^2 a}{V^2} \right) (V - nb) = nRT$$

$a, b$  are given constants, depending on the strength of interactions b/w molecules.

Closer look at the connection b/w microscopic behavior (that of single gas molecule  $\rightarrow$  and its transfer of momentum to the container) and the macroscopic property of the gas (such as its temperature, pressure)

Mechanics for a gas molecule  $\rightarrow$  a particle of mass  $m$



System: one gas molecule + container  $\rightarrow$  no net external force on this system in x ( $\rightarrow$  what about  $mg$ ? same in ①, ②, ③  $\rightarrow$  will not change our result)  $\rightarrow$  motion along perpendicular directions are independent

(8)

Newton's 2<sup>nd</sup> Law:  $F_{net,x} = \frac{dp_x}{dt}$

$$0 = \frac{dp_x}{dt} \rightarrow p_x \text{ is conserved}$$

$\downarrow$  total  
 $m v_{xT}$ : linear momentum  
in the  $x$ -direction.

$$(m v_x)_{(1)} = (m v_x)_{(3)}$$

Total linear momentum = Total linear momentum  
@ (1) @ (3)

$$\underbrace{m v_x}_{\substack{\text{gas} \\ \text{molecule}}} + \underbrace{M \cdot 0}_{\substack{\text{mass of} \\ \text{container}}} = \underbrace{-m v_x}_{\substack{\text{l.m. gas} \\ \text{molecule}}} + \underbrace{2 m v_x}_{\substack{\text{linear momentum} \\ \text{of container}}} = M V_{xc} \rightarrow V_{xc} = \frac{2(m/M)}{1 \text{kg.}} v_x \approx 0$$

Conclusion: after hitting right wall, a gas molecule has transferred  $2m v_x$  (momentum) to the container.

$$\downarrow P_i = \frac{F_i}{A} = \frac{\frac{dp_i}{dt}}{A} = \frac{\frac{2m v_x}{\frac{2l}{v_x}}}{A} = \frac{m v_x^2}{A \cdot l} = \frac{m v_x^2}{\text{vol.}}$$

$$\downarrow \text{Pressure due to } N \text{ molecules: } P = \sum_{i=1}^N P_i = \frac{m}{\text{vol}} \sum_{i=1}^N v_{xi}^2$$

$$P = \frac{m N}{\text{vol}} \left\{ \frac{\sum_{i=1}^N v_{xi}^2}{N} \right\} \rightarrow P = \frac{m N}{\text{vol}} \overline{v_x^2}$$

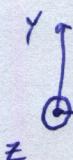
$\overbrace{\text{average of } v_x^2 \rightarrow \overline{v_x^2}}$

$$PV = m N \overline{v_x^2} \quad \overbrace{\text{and } v_x \text{ is one of the 3 components of } \vec{v}} \rightarrow \overline{v_x^2} = \frac{\overline{v^2}}{3}$$

$$PV = mN \frac{\bar{v^2}}{3}$$

$$\bar{v_x^2} = \frac{\bar{v^2}}{3}$$

The av. of  $v^2$  in one direction is the average of  $v^2$  in 3D divided by 3



$x$  &  $z$  are equivalent.

$\bar{v_y} \rightarrow$  there is molecule weight of mg since  $m \sim 10^{-27}$  kg, for this derivation, we assume it is negligible  
 $\rightarrow x, y, z$  are equivalent.

Now relate this to the eq-of state for an ideal gas:  $PV = kNT$

$$kN\bar{T} = mN \frac{\bar{v^2}}{3} \rightarrow kT = \frac{1}{3}m\bar{v^2}$$

$$3kT = m\bar{v^2}$$

$$\frac{3}{2}kT = \frac{1}{2}m\bar{v^2}$$

proportional to temp.  
 ↓  
 Macroscopic

Average kinetic energy for one molecule.  
 ↓  
 Microscopic

Recall: Temperature: a macroscopic property that is a consequence of microscopic behavior

→ We can use reverse connection as well:

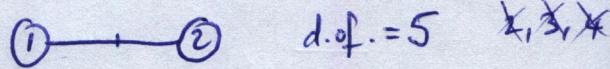
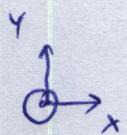
$$\text{Room } \begin{cases} T_1 = 298 \text{ °K (normal condition)} \\ T_2 = 320 \text{ °K} \end{cases} \Rightarrow \frac{1}{2}m\bar{v_1^2} < \frac{1}{2}m\bar{v_2^2}$$

## Dimensions :

$$\left\{ \begin{array}{l} 3D \longrightarrow \frac{3}{2} kT = \frac{1}{2} m v^2 \\ 1D \rightarrow \text{What is the average KE per molecule in } 1D \rightarrow \frac{1}{2} kT \\ 2D \rightarrow kT \end{array} \right.$$

↳ av. KE of a gas molecule per degree of freedom is  $\frac{1}{2} kT$ .

↳ Molecule formed of 2 atoms that are connected:  
 $O_2, N_2, \text{etc.}$

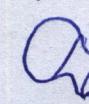


$$\left\{ \begin{array}{l} ① \rightarrow \text{d.o.f.} : 3 \\ ② \rightarrow \text{d.o.f.} : 3 \\ ① \quad ② \rightarrow \text{d.o.f.} = 6 \end{array} \right.$$

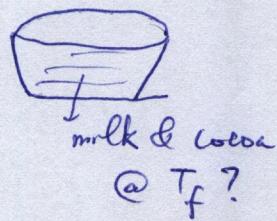
$x$ : ① moves left  $\rightarrow$  so will ②  
 $y$ : ① moves up, ② not necessarily will move up  
 $z$ : ① moves out of pipe  
 ② not necessarily will move out of pipe  
 (can rotate with middle pivot)

$$\left\{ \begin{array}{l} \text{Av. KE per diatomic molecule is } \frac{5}{2} kT \\ \text{Av. KE per monoatomic molecule is } \frac{3}{2} kT \end{array} \right.$$

16-54

milk  $m_m = 2 \text{ oz}$   
  
 $T_m = 3^{\circ}\text{C}$   
 $T_c = 90^{\circ}\text{C}$   
 cocoa  $m_c = 6 \text{ oz}$

$$C_m = C_c = C_{water} = 4184 \frac{\text{J}}{\text{kg} \cdot \text{K}}$$



$$\text{Heat balance equation: } \Delta Q_c + \Delta Q_m = 0$$

$$(\text{isolated system}) \quad m_c c_c (T_f - T_c) + m_m c_m (T_f - T_m) = 0$$

CW

$$(m_c c_w + m_m c_w) T_f = m_c c_w T_c + m_m c_w T_m$$

$$T_f = \frac{m_c T_c + m_m T_m}{m_c + m_m}$$

$m \rightarrow \text{in kg}$  (not necessary in this particular eq.)  $\Rightarrow$  masses showing above & below the

$$T_f = \frac{6 \times 363.16 + 2 \times 276.16}{8} = 341.46 \text{ } ^\circ\text{K}$$

$$\text{Can go back to celcius: } T_f = 341.46 - 273.16 = 68.3^\circ\text{C}$$

If I work in ~~the~~ claims:

$$T_f = \frac{m_c(T_{c_k} - 273.16) + m_m(T_{m_k} - 273.16)}{m_c + m_m}$$

$$= \frac{m_c T_{ck} + m_m T_{mk}}{m_c + m_m} + \frac{(m_c + m_m)(-273.16)}{(m_c + m_m)}$$

$$T_f = T_{fK} - 273.16$$

## Conversion factors (Appendix C)

$$1 \text{ oz} = 0.02835 \text{ kg}$$

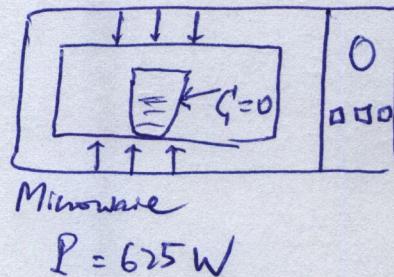
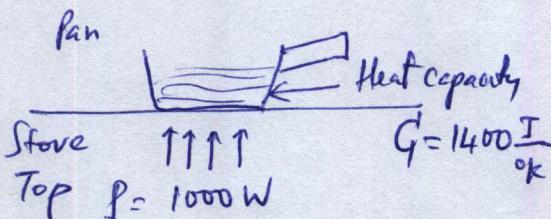
$$1 \text{ lb} = 0.454 \text{ kg}$$

$$1 \text{ in} = 0.0254 \text{ m}$$

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116.49

- 1) Write down the data
- 2) Write down the equation
- 3) Solve for what is needed



Heat capacity:  $C = c \cdot m$

$\downarrow$        $\downarrow$   
specific mass

Relating to what we said:  $\Delta Q = mc \Delta T = C \Delta T$

Question: How much water before it is quicker to heat using stove top? shorter time

Let's compare time it takes to heat an amount of water  $M$  so its temp increases  $\Delta T$ , using stove top & microwave

stove top $\Delta t_s ?$ 

$$H_s = \frac{\Delta Q}{\Delta t_s}$$

↓  
heat transfer  
per unit time

" 1000 W

$$\rightarrow \Delta t_s = \frac{\Delta Q}{1000} = \frac{(C_w + C_{pan}) \Delta T}{1000}$$

Heat transferred from  
stove top (@ 1000  $\frac{J}{s}$ )  
is absorbed by pan  
& water

$$C_{pan} = 1400 \frac{J}{^{\circ}K}$$

$$C_w = 4184 \frac{J}{kg \cdot ^{\circ}K}$$

$$C_w = m_w C_w$$

$$\Delta t_s = \frac{(m_w C_w + C_{pan}) \Delta T}{1000}$$

Microwave $\Delta t_m ?$ 

$$H_m = 625 \frac{J}{s} = 625 W$$

$$\Delta t_m = \frac{\Delta Q}{625} = \frac{C_w \Delta T}{625}$$

↓  
Heat transferred in from  
microwave is  
absorbed by water  
(paper up has  $C \approx 0$ )

$$\Delta t_m = \frac{m_w C_w \Delta T}{625}$$

When is it quicker w/ stove top?

$\Delta t_s < \Delta t_m$  @ what  $m_w$ ?

$$\frac{(m_w C_w + C_{pan}) \Delta T}{1000} < \frac{m_w C_w \Delta T}{625}$$

$$\frac{C_{pan}}{1000 C_w 0.375} < m_w \left( \frac{C_w}{625} - \frac{C_w}{1000} \right) = m_w C_w (0.375)$$

$$\frac{C_{pan}}{1000 C_w 0.375} < m_w$$

$$\frac{1400}{375 \times 4184} = [0.558 \text{ kg} < m_w]$$

a)

b) Rate of temperature increase? or  $\frac{\Delta T}{\Delta t}$

$$m_w = 0.558 \text{ kg} \rightarrow \Delta t_s = \frac{m_w c_w + C_{pan}}{1000} \Delta T \rightarrow \frac{\Delta T}{\Delta t_s} = \frac{1000}{m_w c_w + C_{pan}}$$

$$\frac{\Delta T}{\Delta t_s} = \frac{1000}{0.558 \times 184 + 1400} = 0.268 \frac{^{\circ}\text{K}}{\text{s}}$$

## Thermal Behavior of Matter (Cont.)

(B)

When heat is supplied to matter, what are the

( $\Delta Q$ )

↓  
delta  $\leftrightarrow$  increment or  
change of

Consequences?

1)  $\Delta T$  ( $\Delta Q$  produces a change of temp.):

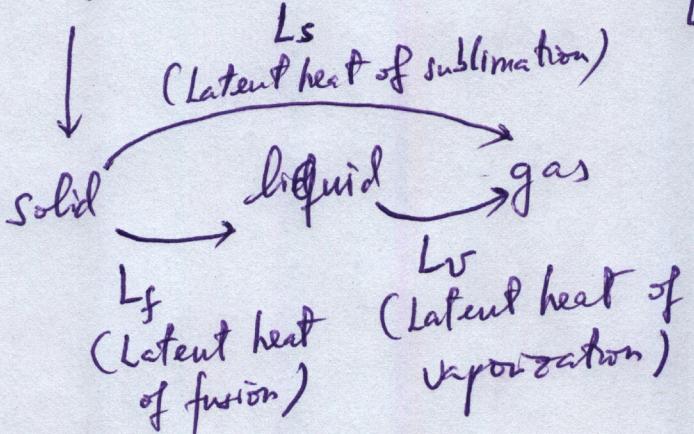
$$\Delta Q = mc \Delta T$$

$$\frac{\Delta L}{L}$$

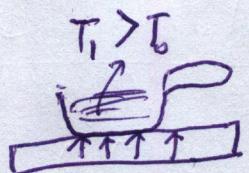
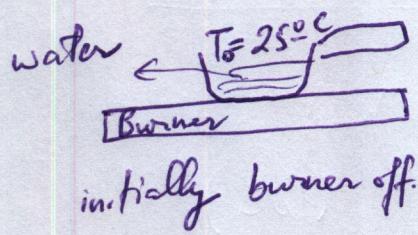
2) Expansion:

- Linear expansion coefficient  $\alpha = \frac{\Delta L}{L}$   
( $L$ : length,  $T$ : temp.)
- Volumic expansion coefficient  $\beta = \frac{\Delta V}{V}$   
( $V$ : vol,  $T$ : temp.)

3) Change of phase:  $\Delta Q = m \frac{L}{\downarrow}$   
"Latent heat"



(16)

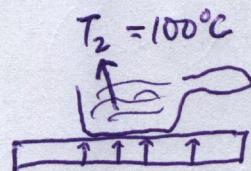


burner on

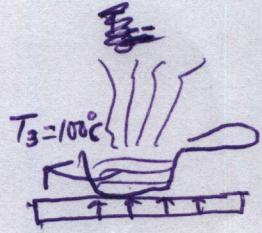
$$\Delta Q = mc \Delta T$$

$$(T_1 - T_0)$$

Heat supplied  
↓  
increase in  
temperature



water starts  
to boil



some of water  
evaporates :  
Change of phases  
vaporization

$$\Delta Q = m L_v$$

water temp. max is  $100^\circ\text{C}$ !  
there is  $\Delta T = 0$  ~~f~~  
since water starts boiling  
until it evaporates.  
(Note the different equation  
to use in a change of  
phase!)

Table 17-1 :

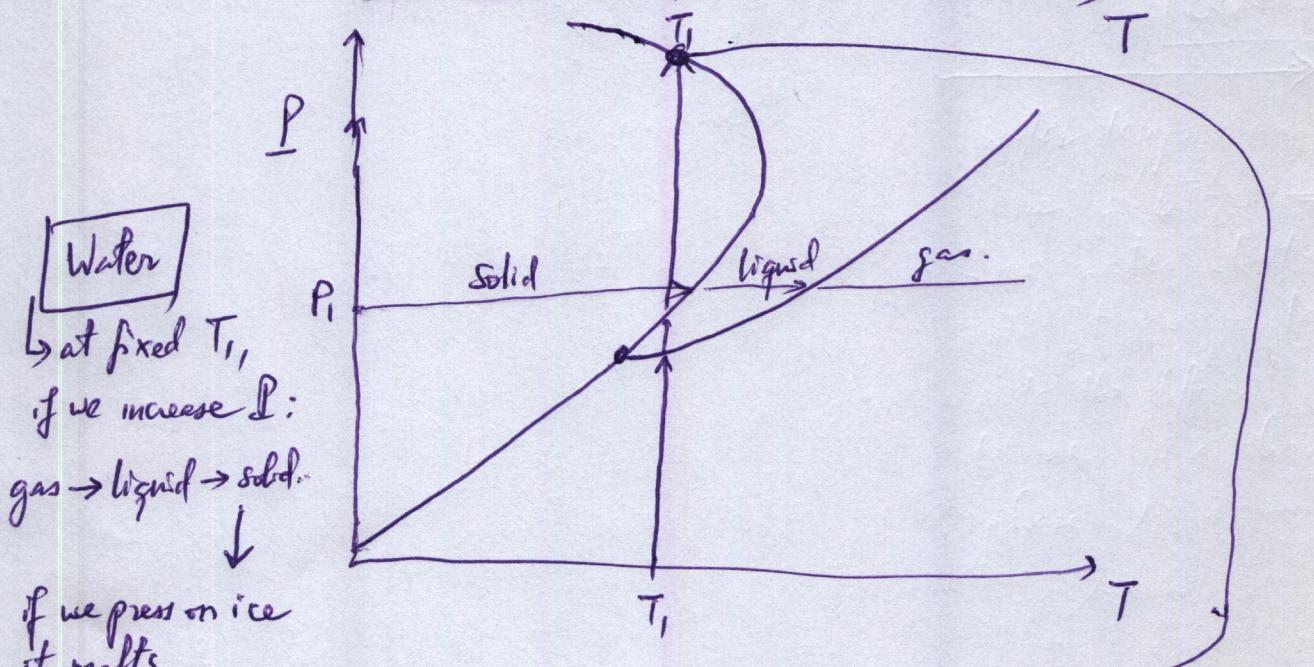
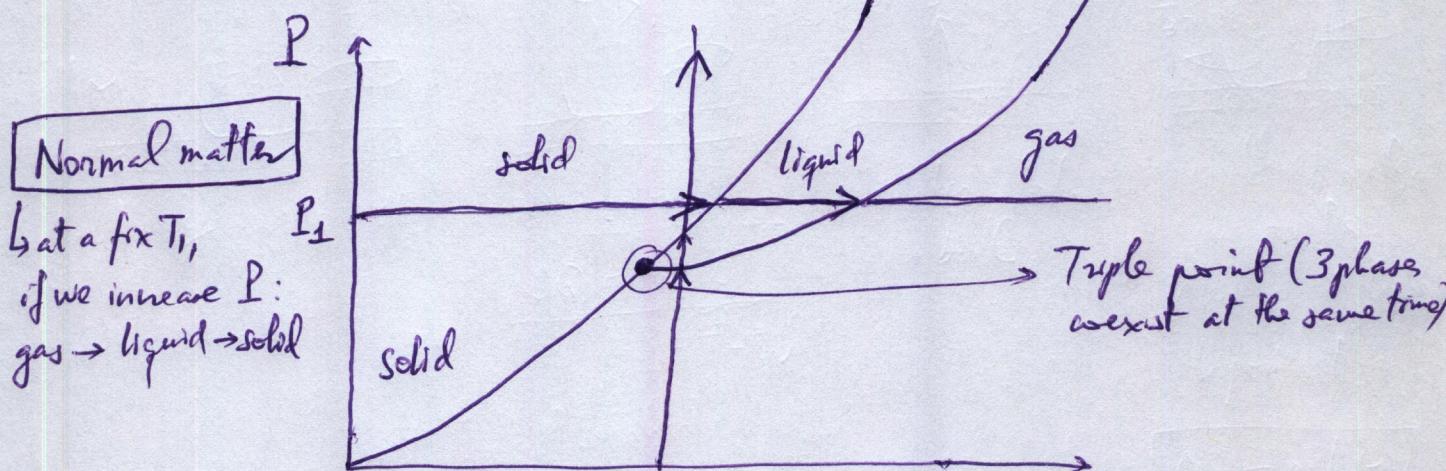
Water:

$$L_f = 334 \frac{\text{kJ}}{\text{kg}}$$

(it takes 334 kJ to melt  
one kg of ice)

$$L_v = 2257 \frac{\text{kJ}}{\text{kg}}$$

Phase diagram:  $P$  vs.  $T$ .



(ice skates melt the ice!)

@ this point (fixed  $T_1$ ) if we increase  $P$  further, solid goes back to liquid!

# (18)

## Ch 18: Heat, Work, 1<sup>st</sup> Law of Thermodynamics.

1<sup>st</sup> Law of Thermodynamics:

$$\rightarrow \Delta U = Q - W$$

Conservation of energy

Heat absorbed by a system:  $Q$

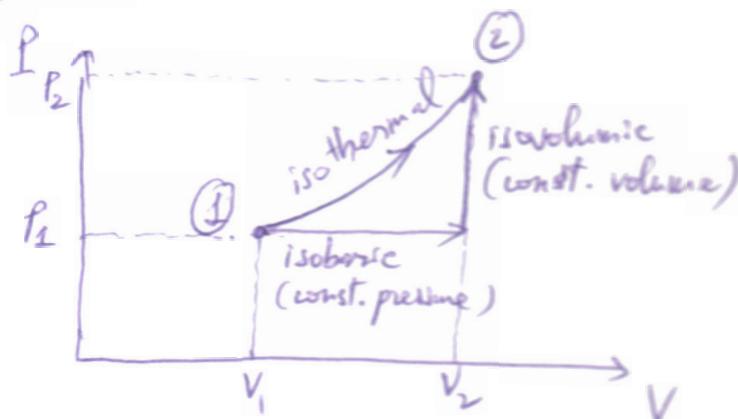
Work done by system:  $W$

Change of internal energy of system:  $\Delta U$

$$\Delta U = Q - W$$

State      not state      variables  $\rightarrow$  they depend on a particular process.  
 variable  
 (does not depend on process)

**State**: is a point on a P,V diagram. We have set values for P & V in a state.



Alternatives ①  $\rightarrow$  ②

- 1) Isobaric + Isochoric
- 2) Isothermal: constant temp.

**Process**: connects two different stats.

$\Delta U_{12}$  or change of internal energy of a system b/w ① & ② is the same whether the system went from ① to ② via isobaric + isochoric or via an isothermal process.

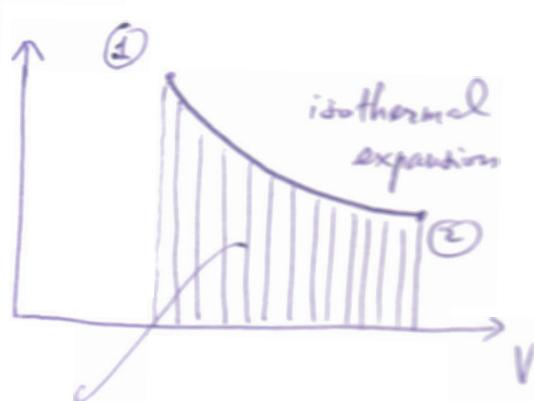
$Q$  &  $W$  b/w ① & ② individually depend on the particular process!

(1a)

Work done by a system:  $W = \int P dV$

(Recall:  $P = \frac{F}{A}$ ;  $W = F \cdot \Delta x = P \cdot \frac{A \cdot \Delta x}{\Delta V}$ )

In a PV diagram:



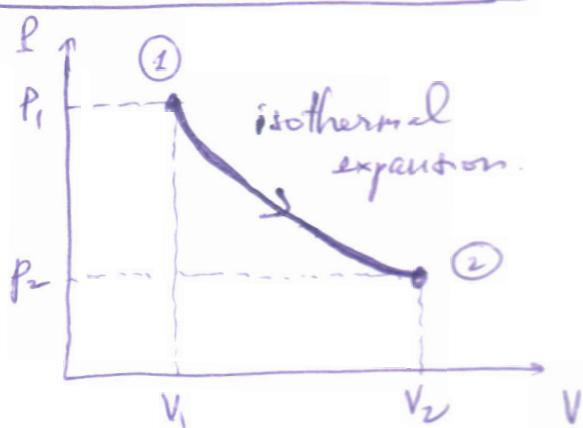
$\int P dV$  is the area under the curve  
→ Work done is this area.

Processes:

- 1) Isothermal ( $T$  is const.)
- 2) Isovolume ( $V$  is const.)
- 3) Isobaric ( $P$  is const.)
- 4) Adiabatic (no heat is absorbed:  $Q=0$ )

Since  $Q$  &  $W$  depend on a particular process:

Isothermal ( $T$  is const.)



$$W = \int_1^2 P dV = nRT \int_1^2 \frac{dV}{V} = nRT \left[ \ln V \right]_1^2$$

Ideal gas

$$\bar{N} = nRT$$

constant in  
isothermal  
processes!

$$W = nRT \left( \ln V_2 - \ln V_1 \right) = nRT \ln \left( \frac{V_2}{V_1} \right)$$

To find  $Q$  we will find  $\Delta U$  in an isothermal process, then use the 1st Law of Thermodynamics:  $\Delta U = Q - W \rightarrow Q = \Delta U + W$

What is  $\Delta U$  in an isothermal process on ideal gas?

Ideal gas: 1)  $\leftrightarrow$  no interaction b/w molecules  $\leftrightarrow$  no potential energy  $\leftrightarrow$  total internal energy comes from kinetic energy only ( $E = \frac{1}{2}mv^2 + P.E.$ )

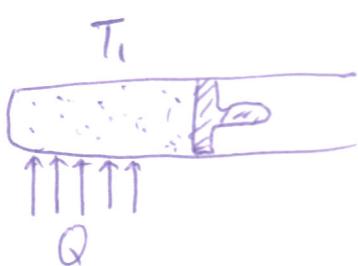
2) Av. KE per molecule in an ideal gas is proportional to the temperature  $\left\{ \begin{array}{l} \frac{3}{2}kT \text{ (mono-atom)} \\ \frac{5}{2}kT \text{ (diatom)} \end{array} \right.$

$$3) \Delta U_{12} = U_2 - U_1 = \left\{ \begin{array}{l} \frac{3}{2}k(T_2 - T_1) = 0 \\ \frac{5}{2}k(T_2 - T_1) = 0 \end{array} \right\} = 0$$

①  $\rightarrow$  ②  
const. T  
 $T_2 = T_1$

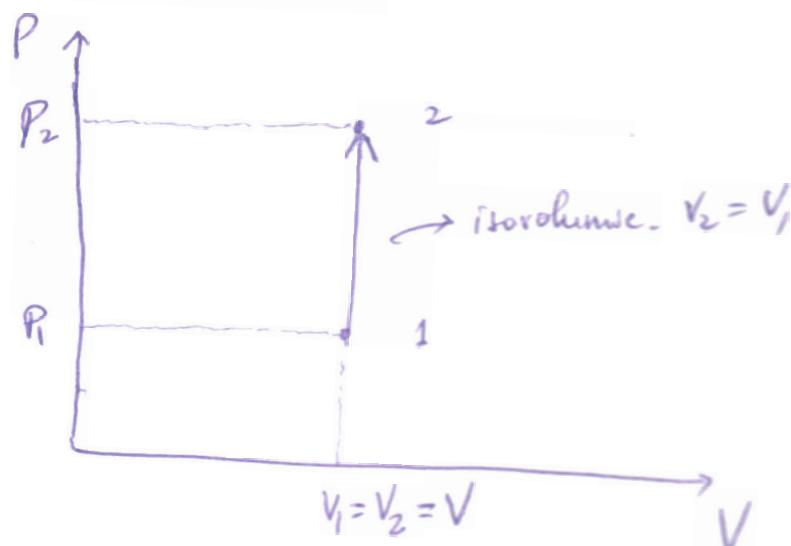
$\boxed{\Delta U = 0 \text{ in any isothermal process}}$

$\Rightarrow \boxed{Q = W}$  In an isothermal process the heat absorbed is equal to work done since  $\Delta U = 0$



$$W = Q \text{ if } T_1 = T_2$$

Isovolumic (const. V)



$$W = \int_1^2 P dV = 0$$

1<sup>st</sup> Law of TD :  $\Delta U = Q - W \rightarrow Q = \Delta U$

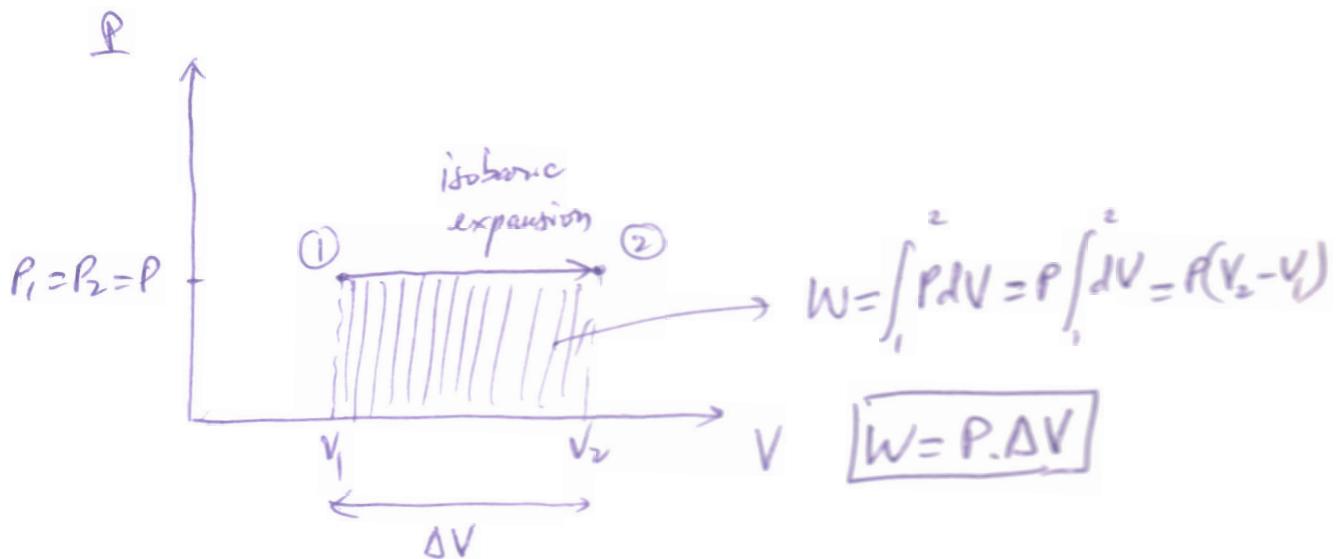
What is  $\Delta U$  in an isovolumic process in ideal gas?

↓  
 $c_v$  : specific heat at constant volume

$$C_V \equiv \frac{1}{n} \frac{Q}{\Delta T} \stackrel{\downarrow}{=} \frac{1}{n} \frac{\Delta U}{\Delta T}$$

$Q = c_v n \Delta T = \Delta U$

## Isobaric Process (const P.)



What is  $Q$ ?

$c_p$  : specific heat @ const.  $P$  :  $c_p = \frac{1}{n} \frac{Q}{\Delta T}$

$$Q = c_p n \Delta T$$

Ideal gas:

$$\underline{PV = nRT}$$

$W$   
(isobaric)

1st Law of TD:  $\Delta U = Q - W$

$$\begin{array}{c} \downarrow \\ nC_V \Delta T \end{array} \quad \begin{array}{c} \downarrow \\ nC_P \Delta T \end{array} \quad \begin{array}{c} \downarrow \\ nR \Delta T \end{array} \rightarrow$$

$$C_V = C_P - R$$

$$\boxed{C_p = C_v + R}$$

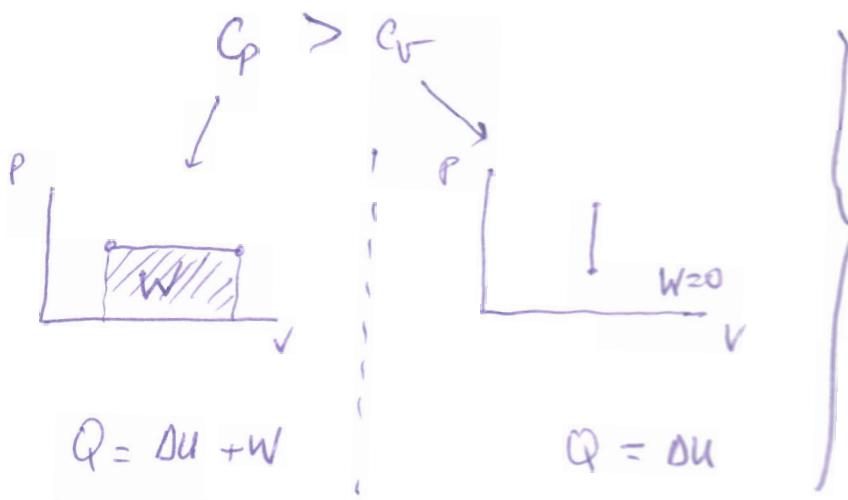
This is a connection  
b/w a isobaric &  
isovolumic process

$$R = 8.314 \frac{\text{J}}{\text{mol} \cdot \text{K}}$$

$$C_p > C_v$$

More heat absorption  
capacity @ constant  $P$   
than @ constant volume

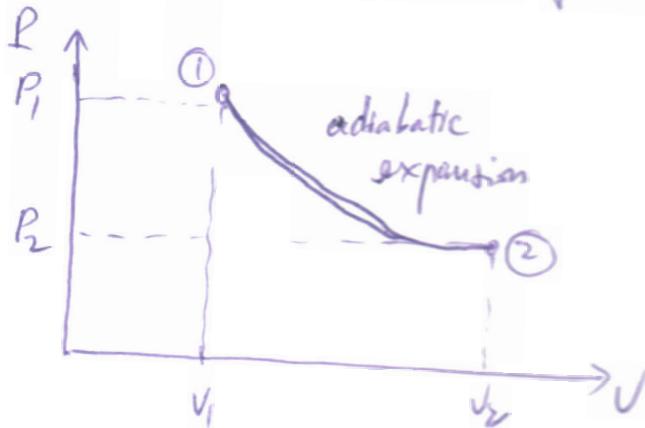
(23)



A system can absorb more heat @ constant  $P$  since it can do work (but not in a isovolumic process!)

Adiabatic Process : ( $Q = 0$ )

$$W = -\Delta U \quad (1^{\text{st}} \text{ law of TD: } \Delta U = Q - W)$$



$$W = \frac{P_1 V_1 - P_2 V_2}{\gamma - 1}$$

dimensionless coefficient

$$\gamma = \frac{C_p}{C_v}$$

$\gamma$  depends on the type of gas : monoatomic or diatomic :

$$C_v = \frac{1}{n} \frac{\partial U}{\partial T} = \begin{cases} \text{monoatomic} : \frac{1}{n} \frac{N \frac{3}{2} k T}{\partial T} = \frac{3 k}{2} \frac{N}{n} = \frac{3}{2} k N_A = \frac{3}{2} R \\ \text{diatomic} : \frac{5}{2} R \end{cases}$$

$$U = N \frac{3}{2} k T$$

(Total internal energy for an ideal monoatomic gas)

$$N = \text{total \# of molecules}$$

$$n : \# \text{ of moles} = \frac{N}{N_A}$$

$$N_A = 6.022 \times 10^{23}$$

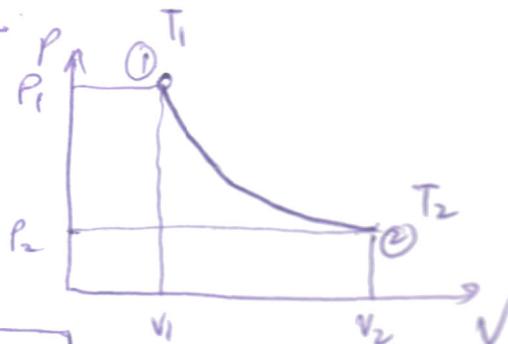
$$k : \text{Boltzmann const.} = 1.38 \times 10^{-23} \frac{\text{J}}{\text{K}}$$

$$R = k N_A = 8.314 \frac{\text{J}}{\text{mol K}}$$

$$\gamma = \frac{C_p}{C_v} = \frac{C_v + R}{C_v} =$$

$$\gamma = \begin{cases} \text{Monoatomic} : \frac{\frac{3}{2} R + R}{\frac{3}{2} R} = \frac{5}{3} = 1.67 \\ \text{Diatomic} : \frac{\frac{5}{2} R + R}{\frac{5}{2} R} = \frac{7}{5} = 1.4 \end{cases}$$

Adiabatic process:



$P_1 V_1 \neq P_2 V_2$  since  $T_1 \neq T_2$

$$P_1 V_1^\gamma = P_2 V_2^\gamma$$

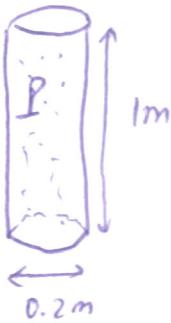
also because  $PV = nRT \Rightarrow P = \frac{nRT}{V}$

$$nR \frac{T_1}{V_1} V_1^{\gamma-1} = nR \frac{T_2}{V_2} V_2^{\gamma-1} \leftrightarrow$$

$$T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1}$$

Apply to an ideal gas in an adiabatic process.

17.39



@  $T = 25^\circ\text{C}$  (room temp.)  $\rightarrow P = 180 \text{ atm.}$

a) How many moles of air  $n$

$$\text{Assume ideal gas: } n = \frac{PV}{RT}$$

$$P = 180 \text{ atm.} \cdot \frac{1.013 \times 10^5 \text{ Pa}}{1 \text{ atm.}}$$

$$V = \pi (0.1)^2 \cdot 1 = \frac{\pi}{100} \text{ m}^3$$

$$R = 8.314 \frac{\text{J}}{\text{K mol}}$$

$$T = 25 + 273.16 = 298.16^\circ\text{K}$$

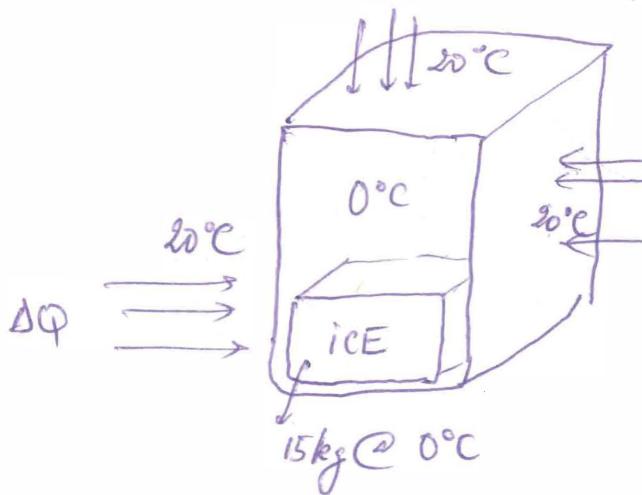
$$n = \frac{180 \times 1.013 \times 10^5 \times \frac{\pi}{100}}{8.314 \times 298.16} = 231 \text{ mol}$$

b) What would be the gas volume @  $P = 1 \text{ atm}$  &  $T = 25^\circ\text{C}$   
 $\rightarrow n = 231 \Rightarrow \frac{PV}{RT}$  { if  $P$  decreases 180 fold  
 $\rightarrow V$  increases 180 times}

$$V = \frac{12}{100} \times 180 \text{ m}^3 = 5.65 \text{ m}^3$$

(17.65)

Thermal resistance of Fridge wall is  $R = 0.12 \frac{\text{°K}}{\text{W}}$



Fridge:  $\rightarrow \Delta Q$

Heat will come in through walls  
only delayed by Thermal resistance R

$$R = \frac{R}{A} \rightarrow R\text{-factor}$$

area

$R \rightarrow$  determine H (Heat transfer rate through fridge's walls)

$$\rightarrow \text{how long will last } \Delta t = \frac{\Delta Q}{H} \quad (H = \frac{\Delta Q}{\Delta t})$$

$\Delta Q$  will go into melting the ice or  $m_{\text{ice}} L_f$

$$H = -KA \frac{\Delta T}{\Delta x} = -\frac{A \Delta T}{R} = -\frac{A \Delta T}{R A} = -\frac{\Delta T}{R}$$

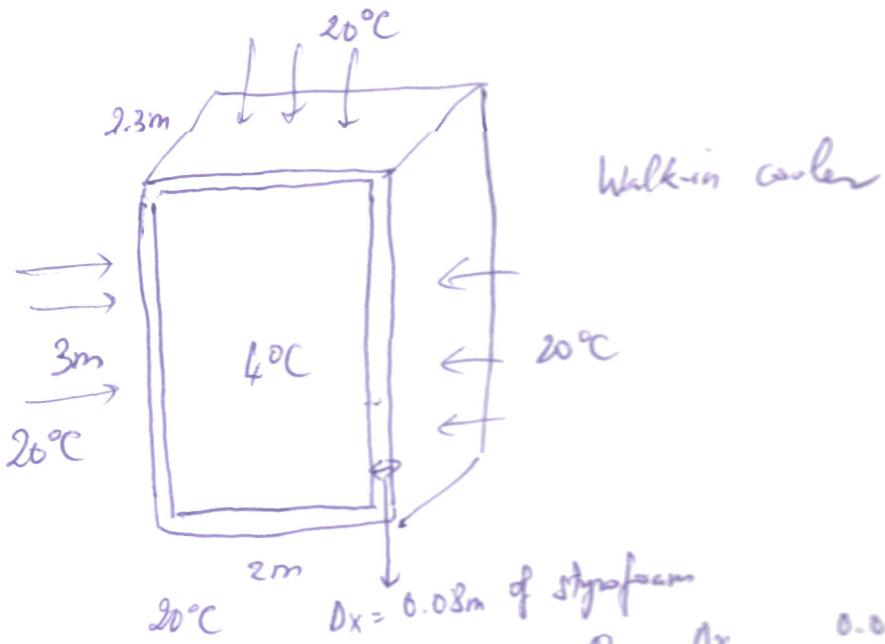
(Heat transferred from outside to inside  $\rightarrow H_{\text{absorbed}} = \frac{\Delta T}{R}$ )

$$\rightarrow \Delta t = \frac{\Delta Q}{H_{\text{abs}}} = \frac{m_{\text{ice}} L_f}{\frac{\Delta T}{R}} = \frac{15 \times 334 \times 10^3}{\frac{(20-0)}{0.12}} = 3 \times 10^4 \text{ s} \frac{1 \text{ h}}{3600 \text{ s}} \\ = 8.35 \text{ h.}$$

$$L_f (\text{water}) = 334 \frac{\text{kJ}}{\text{kg}}$$

20

16.56



$D_x = 0.08\text{ m}$  of styrofoam

$$H = - \frac{A \Delta T}{R}$$

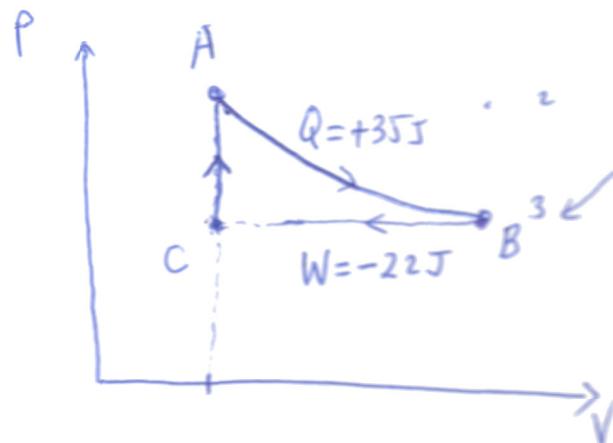
$$\left. \begin{aligned} R &= \frac{D_x}{k} = \frac{0.08}{0.029} = 2.76 \\ \text{Table 16-2} \end{aligned} \right\}$$

$$A = \underbrace{3 \times 2 \times 2}_{\text{Front \& back}} + \underbrace{3 \times 2.3 \times 2}_{\text{Left \& right}} + 7 \cdot 3 \times 2 \times 2 \\ = 35\text{ m}^2$$

$$\boxed{H = - \frac{32 \times 16}{2.76} = - 203\text{ W}}$$

18-42

a)



$$PV = nRT$$

$$P = \frac{nRT}{V}$$

isothermal expansion  
 $A \rightarrow B$   
 (a curve!)

\* expansion  $A \rightarrow B$

(B will be on the right of A)

Incorporate correct signs by comparing data with definitions of  $Q$  &  $W$

$$\Delta U = Q - W$$

Work done by system } Work done  $\rightarrow +$

Heat absorbed

Work received  $\rightarrow -$

+

(Heat coming into system  $\rightarrow$  positive  
 Heat coming out of system  $\rightarrow$  negative)

\* isobaric compression  $B \rightarrow C$

(C will be to the left of B)

on a horizontal line, with  $V_c = V_A$

b) Work done or received by gas during complete cycle:

$$A \rightarrow B \rightarrow C \rightarrow A$$

$$\downarrow \quad \downarrow \quad \downarrow$$

$$W_{AB} \quad W_{BC} \quad W_{CA} = 0 \quad (V_c = V_A \rightarrow \Delta V = 0 \rightarrow W = 0)$$

Work  $W$  and heat  $Q$  are not state variables!  $\rightarrow$  depend on the type of process.

$A \rightarrow B$ : isothermal process:  $W_{AB} = Q$  ( $\Delta U = 0$   
ideal gas)  
 $= +35 \text{ J}$  (given).

$B \rightarrow C$ : isobaric compression:  $W_{BC} = -22 \text{ J}$  (given)

$$W_{ABC A} = W_{AB} + W_{BC} = 35 \text{ J} - 22 \text{ J} = 13 \text{ J}$$

By the sign  $\rightarrow$  work done by gas in one cycle is  $13 \text{ J}$ .

c) (1<sup>st</sup>)  $Q_{BCA} = Q_{ABC A} - Q_{AB}$  (linear superposition)

$$\left\{ \begin{array}{l} Q_{ABC A} = ? \\ \text{DU is a state variable} \rightarrow \Delta U_{ABC A} = 0 \\ \text{1st Law: } \Delta U_{ABC A} = Q_{ABC A} - W_{ABC A} \\ 0 = Q_{ABC A} - 13 \text{ J} \end{array} \right.$$

$$\boxed{Q_{ABC A} = 13 \text{ J}}$$

$$Q_{AB} = +35 \text{ J}$$

$$\rightarrow Q_{BCA} = 13 \text{ J} - 35 \text{ J} = -22 \text{ J}.$$

By the sign heat in the amount of  $22 \text{ J}$  has been lost by the gas in  $B \rightarrow C \rightarrow A$ .

(2<sup>nd</sup>)  $Q_{BCA} = Q_{BC} + Q_{CA}$

## Ch 19 2<sup>nd</sup> Law of Thermodynamics

In connection with heat engines working b/w 2 different heat reservoirs.

Heat reservoir : a source of heat, large, at constant temp.

Visual experiment: put a piston filled with an ideal gas in thermal contact with a heat reservoir (hot) at temperature  $T_h$ . Gas absorbs heat, expands, does work. No more expansion (no more work done) when gas reaches same temp. as the constant  $T_h$  heat reservoir. How to get more work done?  $\rightarrow$  Bring gas back to its original temp. by putting it in thermal contact with a cold reservoir @ temp.  $T_c \rightarrow$  gas loses heat, compressed (receiving work).

Diagrams:

Gas does work :



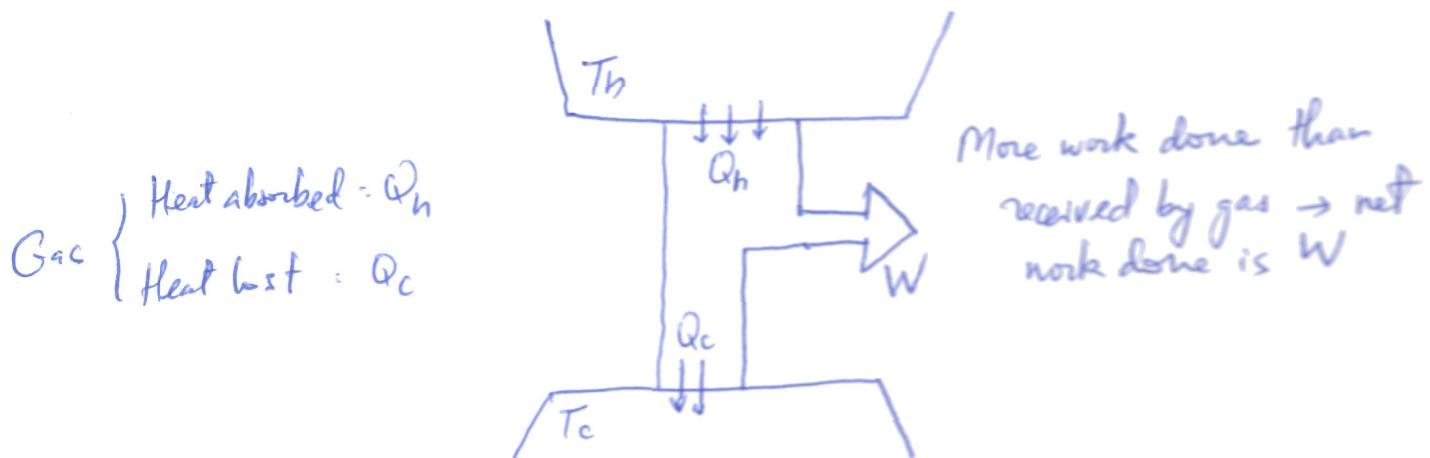
(1<sup>st</sup> half of cycle)

Gas receives work:



(2<sup>nd</sup> half of cycle)

In one diagram: Heat engine



1<sup>st</sup> Law of T.D. for a heat engine:

$$\underbrace{\Delta U}_0 = Q_{\text{net}} - W = Q_h - Q_c - W$$

In one complete cycle

(the 2nd half brings gas back to original condition or state)

$$Q_h - Q_c = W$$

Efficiency of the heat engine:  $e = \frac{W}{Q_h} = \frac{Q_h - Q_c}{Q_h} = 1 - \frac{Q_c}{Q_h}$

$$0 < \frac{Q_c}{Q_h} < 1$$

$$\rightarrow e = 1 - \frac{|Q_c|}{|Q_h|} < 1$$

There is not  $e > 1$

↓ 2<sup>nd</sup> Law of T.D.: it is impossible to build a heat engine operating in cycles that extracts heat from a hot reservoir (and returning some of it to a cold reservoir) that can deliver 100% efficiency ( $e < 1$ )

18.59, 33, 17.71

(18.59)

Gas mixture: Ar & O<sub>2</sub>  
 Fraction: f 1-f

(0 < f < 1)

$$\begin{cases} V_1 \rightarrow V_2 = 2V_1 \\ P_1 \rightarrow P_2 = \frac{P_1}{3} \end{cases}$$

Adiabatic process (expansion)

Possible paths: Q=0 X

ΔU = -W X

$$P_1 V_1^{\gamma} = P_2 V_2^{\gamma} \checkmark \quad \gamma = \frac{C_p}{C_v} = \frac{C_N + R}{C_v} = 1.4$$

$$C_v = \frac{3}{2} R f + \frac{5}{2} R (1-f)$$

monoatomic    diatomic.

$$\gamma = \frac{\frac{3}{2} R f + \frac{5}{2} R (1-f) + R}{\frac{3}{2} R f + \frac{5}{2} R (1-f)} = \frac{\frac{7}{2} - f}{\frac{5}{2} - f}$$

Now find γ:

$$\frac{P_1}{P_2} = \left( \frac{V_2}{V_1} \right)^{\gamma} \rightarrow \ln \left( \frac{P_1}{P_2} \right) = \gamma \ln \left( \frac{V_2}{V_1} \right)$$

$$\rightarrow \gamma = \frac{\ln \left( \frac{P_1}{P_2} \right)}{\ln \left( \frac{V_2}{V_1} \right)} = \frac{\ln 3}{\ln 2} = 1.58$$

(recall: monoatomic:  $\gamma = 1.67$ ; diatomic  $\gamma = 1.4$ )

$$\frac{5}{2} \gamma - \gamma f = \frac{7}{2} - f \rightarrow \frac{5}{2} \gamma - \frac{7}{2} = (\gamma - 1)f \rightarrow f = \frac{\frac{5}{2} \gamma - \frac{7}{2}}{\gamma - 1}$$

$$f = \frac{\frac{5}{2} 1.58 - \frac{7}{2}}{1.58 - 1} = 0.78$$

Ar	78 %
O <sub>2</sub>	22 %

18.33

Blood artery pressure

$$\left\{ \begin{array}{l} P_H = 125 \text{ mm Hg} \\ P_L = 80 \text{ mm Hg} \end{array} \right. \begin{array}{l} \text{gauge pressure.} \\ \text{actual pressures} \rightarrow \\ \text{add atmospheric} \\ \text{pressure = 1 atm} \\ \downarrow \\ 760 \text{ mm Hg} \end{array}$$

Air bubble :  $d_L = 1.52 \text{ mm} @ P_L$ a)  $d_H$ ? ( $d_H < d_L$ )  $\rightarrow$  gas volume will determine the diameter of the spherical bubble :

Ideal gas equation:  $PV = nRT$   $\left\{ \begin{array}{l} P_L V_L = nRT \\ P_H V_H = nRT \end{array} \right. \begin{array}{l} \text{same body} \\ \text{temp.} \end{array}$

$$\hookrightarrow P_L V_L = P_H V_H \rightarrow V_H = \frac{P_L}{P_H} V_L$$

$$\frac{4}{3}\pi \left(\frac{d_H}{2}\right)^3 = \frac{P_L}{P_H} \frac{4}{3}\pi \left(\frac{d_L}{2}\right)^3$$

$$d_H^3 = \frac{P_L}{P_H} d_L^3$$

$$d_H = \left(\frac{P_L}{P_H}\right)^{\frac{1}{3}} d_L$$

$$= \frac{(760 + 80)^{\frac{1}{3}}}{(760 + 125)^{\frac{1}{3}}} 1.52 \text{ mm}$$

$$d_H = \left(\frac{840}{885}\right)^{\frac{1}{3}} 1.52 \text{ mm} = 1.49 \text{ mm.}$$

$$760 \text{ mm Hg} \rightarrow 1 \text{ atm} \rightarrow 1.013 \times 10^5 \text{ Pa}$$

b) How much work does blood (so heart) do to compress the bubble? (body temp. stays const. @ 37°C  $\rightarrow$  isothermal process)

$$W = nRT \ln\left(\frac{V_2}{V_1}\right) = \underbrace{nRT}_{P_L V_L} \ln\left(\frac{V_H}{V_L}\right) = \left\{ \begin{array}{l} 840 \cdot \frac{1.013 \times 10^5}{760} \times \frac{4}{3}\pi \left(\frac{1.52 \times 10^{-3}}{2}\right)^3 \times \\ \ln\left[\left(\frac{1.49}{1.52}\right)^3\right] \\ = -12312 \times 10^{-9} \text{ J} \end{array} \right.$$

↓  
Work done on gas or bubble  
since it is getting compressed.

$$= -12 \mu \text{J}$$

 $\downarrow \text{micro or } 10^{-6}$

(17.71)

33

Clock: brass pendulum:  $L = 0.2 \text{ m}$  @  $20^\circ\text{C}$  (good)  
 calibrated to work as a clock @  $20^\circ\text{C}$ .



$T_2 = 18^\circ\text{C} \rightarrow$  how long until it makes a 1 min error?

Since for a pendulum: # oscillations per second  $\omega = \sqrt{\frac{g}{L}}$

Length will change with temp, according to the linear coefficient of expansion for brass:  $\rightarrow$  Table 17.2:  $\alpha = 19 \times 10^{-6} \text{ K}^{-1}$

$$\alpha = \frac{\frac{\Delta L}{L}}{\Delta T} \rightarrow \frac{\Delta L}{L} = \alpha \Delta T \rightarrow \Delta L = \alpha L \Delta T$$

$$T = \frac{2\pi}{\omega} = 2\pi \sqrt{\frac{L}{g}} \quad \left\{ \begin{array}{l} T_{20^\circ\text{C}} = 2\pi \sqrt{\frac{L}{g}} \\ T_{18^\circ\text{C}} = 2\pi \sqrt{\frac{L + \Delta L}{g}} = 2\pi \sqrt{\frac{L + \alpha L \Delta T}{g}} \\ \qquad \qquad \qquad = 2\pi \sqrt{\frac{L(1 + \alpha \Delta T)}{g}} \end{array} \right.$$

$$T_{18^\circ\text{C}} < T_{20^\circ\text{C}} \rightarrow T_{20^\circ\text{C}} - T_{18^\circ\text{C}} = \frac{2\pi}{\sqrt{g}} \left[ \sqrt{L} - \sqrt{L(1 + \alpha \Delta T)} \right] \\ = 2\pi \sqrt{\frac{L}{g}} \left[ 1 - \sqrt{1 - 2\alpha} \right]$$

$\downarrow \Delta T = -2^\circ\text{K}$ .

$$\sqrt{1 - 2\alpha} = (1 - 2\alpha)^{1/2} \approx 1 - \frac{1}{2}(2\alpha) = 1 - \alpha$$

$$(1 + x)^{1/2} \approx 1 + \frac{1}{2}x + \dots$$

negligible if  $x$  very  
small compared to 1

$$\boxed{T_{20^\circ\text{C}} - T_{18^\circ\text{C}} = 2\pi \sqrt{\frac{L}{g}} [1 - (1 - \alpha)] = 2\pi \sqrt{\frac{L}{g}} \alpha}$$

time error per period.

How many periods of pendulum until a difference of 1 min.

$$\frac{60\text{s}}{2\pi\sqrt{\frac{L}{g}}\alpha}$$

How long until a difference of 60s?  $\frac{60\text{s}}{2\pi\sqrt{\frac{L}{g}}\alpha} T_{20^\circ}$

$$= \frac{60}{2\pi\sqrt{\frac{L}{g}}\alpha} \cancel{2\pi\sqrt{\frac{L}{g}}\alpha} \bullet$$

$$\approx \frac{60}{\alpha} = \frac{60}{19 \times 10^{-6}} \text{s} \rightarrow \underline{\underline{36.5 \text{ days}}}$$